

PCT

WORLD INTELLECTUAL PROPERTY ORGANIZATION
International Bureau



INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(51) International Patent Classification ⁶ : A61K 9/51, 9/52, 9/46, 9/56, 9/58, 9/64	A1	(11) International Publication Number: WO 95/27482
		(43) International Publication Date: 19 October 1995 (19.10.95)

(21) International Application Number: PCT/IE95/00025
(22) International Filing Date: 6 April 1995 (06.04.95)
(30) Priority Data: 940292 6 April 1994 (06.04.94) IE
(71) Applicant (for all designated States except US): ELAN CORPORATION, PLC [IE/IE]; Monksland Industrial Estate, Athlone, County Westmeath (IE).
(72) Inventors; and
(75) Inventors/Applicants (for US only): FREEMAN, Virginia [IE/IE]; Tarmon, Castlereagh, County Roscommon (IE). RAMTOOLA, Zebunnissa [IE/IE]; 163 Charlemont, Griffith Avenue, Dublin 9 (IE).
(74) Agent: ANNE RYAN & CO.; 60 Northumberland Road, Ballsbridge, Dublin 4 (IE).

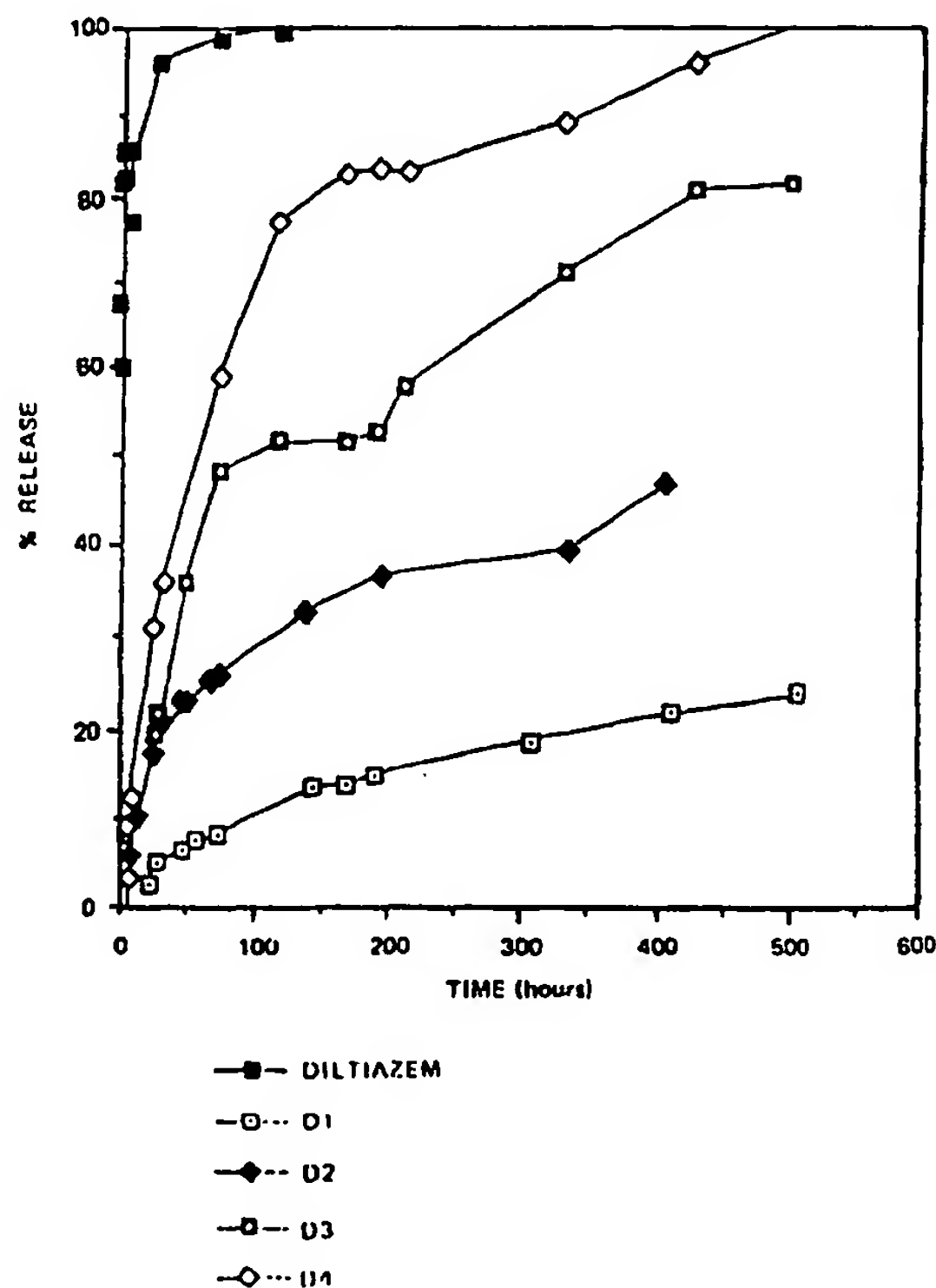
(81) Designated States: AU, CA, JP, NZ, US, European patent (AT, BE, CH, DE, DK, ES, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE).

Published
With international search report.

(54) Title: EFFERVESCENT PHARMACEUTICAL FORMULATIONS CONTAINING CONTROLLED RELEASE BIODEGRADABLE MICROCAPSULES

(57) Abstract

Effervescent pharmaceutical formulations for the sustained and controlled oral administration of a drug selected from a calcium channel blocker, an ACE inhibitor, a narcotic analgesic or analogues or combinations thereof, the formulation comprising microcapsules in which the drug is entrapped in a biodegradable polymer, for example poly-L lactide. The pH of the formulation can be varied to optimize the release of the or each drug from the formulation. Microcapsules suitably have a D 50 % between about 100 nm and 900 nm and a drug loading of the order of about 10 % to 70 % by weight. The formulations can be used to administer the drugs to a patient on a once-daily basis so as to achieve a therapeutic effect over a substantially 24-hour period.



FOR THE PURPOSES OF INFORMATION ONLY

Codes used to identify States party to the PCT on the front pages of pamphlets publishing international applications under the PCT.

AT	Austria	GB	United Kingdom	MR	Mauritania
AU	Australia	GE	Georgia	MW	Malawi
BB	Barbados	GN	Guinea	NE	Niger
BE	Belgium	GR	Greece	NL	Netherlands
BF	Burkina Faso	HU	Hungary	NO	Norway
BG	Bulgaria	IE	Ireland	NZ	New Zealand
BJ	Benin	IT	Italy	PL	Poland
BR	Brazil	JP	Japan	PT	Portugal
BY	Belarus	KE	Kenya	RO	Romania
CA	Canada	KG	Kyrgystan	RU	Russian Federation
CF	Central African Republic	KP	Democratic People's Republic of Korea	SD	Sudan
CG	Congo	KR	Republic of Korea	SE	Sweden
CH	Switzerland	KZ	Kazakhstan	SI	Slovenia
CI	Côte d'Ivoire	LI	Liechtenstein	SK	Slovakia
CM	Cameroon	LK	Sri Lanka	SN	Senegal
CN	China	LU	Luxembourg	TD	Chad
CS	Czechoslovakia	LV	Latvia	TG	Togo
CZ	Czech Republic	MC	Monaco	TJ	Tajikistan
DE	Germany	MD	Republic of Moldova	TT	Trinidad and Tobago
DK	Denmark	MG	Madagascar	UA	Ukraine
ES	Spain	ML	Mali	US	United States of America
FI	Finland	MN	Mongolia	UZ	Uzbekistan
FR	France			VN	Viet Nam
GA	Gabon				

Effervescent pharmaceutical formulations containing
controlled release biodegradable microcapsules

Technical Field

5 This invention relates to effervescent pharmaceutical formulations containing biodegradable controlled release drug-loaded microcapsules. In particular, this invention relates to powder or tablet formulations, particularly once-daily formulations, containing a calcium antagonist, for example, nifedipine, a narcotic analgesic, for example, hydromorphone or an ACE inhibitor, for example, captopril, and the like and analogues
10 or mixtures or combinations thereof.

Background Art

Calcium antagonists and angiotensin converting enzyme (ACE) inhibitors are widely used in patients with cardiovascular disease and are thought to have antihypertensive and vascular protective effects when
15 administered as monotherapy or in combination. Typically, calcium antagonists are used in the treatment of hypertension and chronic stable angina; ACE inhibitors are thought to prevent the development of atherosclerosis and to reduce the number of cardiac ischemic events in patients with coronary artery disease and left ventricular dysfunction.
20 Narcotic analgesics are widely used to provide strong relief of postoperative and chronic pain. However, their clinical usefulness is limited by the development of dependence to their action in the course of chronic treatment. Recently, it has been shown that co-administration of sublingual calcium antagonists and epidural narcotic analgesics
25 potentiate the analgesic effect of the narcotic analgesic and suggested that co-administration might prevent the development of physical dependence on narcotics. (Pereira, *Pain*, 53: 341-355 (1993); Antkiewicz-Michaluk, *Psychopharmacology*, 111:457-64 (1993)). Typically, these drugs are orally administered in tablet/capsule formulations and, in the
30 case of narcotic analgesics, also parenterally administered.

The efficacy of these drugs is improved when they are administered to a subject in a controlled fashion. Normal drug dosing may follow a profile of excessive-ineffective plasma levels whereby the dose initially exceeds the desired therapeutic level, and then falls to subclinical levels. However, controlled/sustained drug delivery can reduce undesirable fluctuations of drug levels, promote therapeutic benefits and minimize toxic effects. Additionally, pre-programmed delivery of a drug in the vicinity of its target cells or to its absorption sites can prevent systemic or side effects involving other tissues.

Thus, there exists a need for pharmaceutically effective, controlled release, targeted formulations containing these drugs or combinations of these drugs.

Microparticulate drug delivery systems based on biodegradable polymers, such as those formed from lactic and glycolic acid, have been widely studied for the controlled/sustained delivery of various drugs. The selection of the particular polymer(s) in light of the particular drug properties, as well as the manufacturing processes and process variables, determine the morphology and size of the microspheres, which in turn influence release characteristics for the formulation. These factors, which sometimes can negate each other, limit the possible formulations and methods for preparation of formulations suitable for controlled/sustained release, including once-daily oral administration.

Effervescent dosage forms incorporating microparticles which are adapted to provide substantially immediate release of the pharmaceutical ingredient contained in the microparticles are disclosed in US 5,178,878 and US 5,223,264.

Disclosure of the Invention

According to the invention, there is provided an effervescent pharmaceutical formulation for the sustained and controlled oral administration of a drug selected from a calcium channel blocker, an ACE inhibitor, a narcotic analgesic or a combination thereof, said

formulation comprising microcapsules in which the drug is entrapped in a biodegradable polymer.

5 The term microcapsule used herein includes the terms "microsphere", "microparticle", "nanosphere" and "nanoparticle". These terms do not necessarily refer to any structural relationship between the drug and the encapsulating polymer (e.g., drug encapsulated within a polymer membrane or drug and encapsulating polymer in a matrix structure). Rather, these terms simply refer to a particle (micron sized or less) in which the drug is entrapped in a polymer.

10 As used herein, the term "sustained/controlled release" refers to a drug release profile designed to optimize delivery of the drug to a particular site(s) of absorption such as the stomach and/or small intestine while still providing effective treatment over a predetermined extended period of time such as once-daily.

15 The oral formulations of this invention are designed to advantageously combine both the benefits of an effervescent or water dispersible tablet with those of a microencapsulated system. For instance, because oral effervescent formulations are easy to administer, they avoid the difficulties associated with chewing or swallowing tablets,
20 thus increasing patient compliance. Incorporation of microcapsules in the oral formulation not only allows targeting of the release of the drug to the absorption site(s) for the drug but also provides a vehicle to control the extent of drug released with respect to time.

25 Further, the drug(s) is encapsulated to form microcapsules which, upon addition of water to the effervescent formulation, are dispersed to produce a fine suspension. Because this uniform suspension is formed prior to the subject ingesting the effervescent drink, the effect of food, presence of bile, pH etc. upon the dissolution of the dosage form is minimized. This is particularly useful for sparingly water soluble drugs
30 such as nifedipine or diltiazem base. Thus, reproducibility of dosing can be improved.

Additionally, for drugs that are not well-absorbed prior to entry into the gastro-intestinal tract, ordinary immediate release effervescent formulations do not protect the drug prior to absorption, thus leading to lessened bioavailability. The addition of microencapsulation to the
5 formula can, however, allow enough flexibility to prevent unwanted release in, for instance, the oral cavity, while promoting delivery of the drug to the targeted area for controlled/sustained release.

A burst effect is common with many microcapsules. Again, if this effect is unwanted in the oral cavity, the formulations of this invention
10 can be designed to minimize (or, if desired, maximize) this burst effect. A particularly effective way to minimize the burst effect is to control the pH of the effervescent drink solution to optimize delivery of the or each encapsulated drug to the targeted absorption sites.

The formulation suitably is used to deliver the drug to a patient on
15 a once-daily basis so as to achieve a therapeutic effect substantially over a 24 hour period.

The microcapsules suitably have a D 50% between about 100 nm and 900 nm, more preferably between about 200 nm and 400 nm.

Further, preferably, the drug loading of the microcapsules ranges
20 from about 10% to 70% by weight, more preferably 20% to 50% by weight.

The invention also provides an effervescent pharmaceutical formulation for the administration of a drug selected from a calcium channel blocker, an ACE inhibitor, a narcotic analgesic or a combination
25 thereof, the formulation comprising drug-loaded biodegradable microcapsules having a D 50% between about 100 nm and 900 nm and a drug loading which ranges from about 10% to 70 % by weight.

Thus the formulations can be used to administer a selected drug to a patient on a once-daily basis so as to achieve a therapeutic effect over a
30 substantially 24 hour period.

Suitable calcium antagonists include diltiazem, verapamil, nifedipine, nimodipine and nicardipine.

Suitable narcotic analgesics include hydromorphone, codeine sulfate, oxycodone, dihydrocodeine tartrate, oxycodone, morphine, fentanyl, sufentanil, oxymorphone and buprenorphine.

Suitable ACE-inhibitors include captopril, enalapril and lisinopril.

The formulations may also include a combination of two or more drugs as hereinbefore specified. Particularly preferred combinations are represented by a combination of a calcium antagonist and a narcotic analgesic. Synergism is displayed by such combinations. A suitable combination comprises nifedipine and hydromorphone.

The polymer matrix suitably comprises polylactide; polyglycolide; poly (lactic acid-co-glycolic acid); poly (ε-caprolactone); poly (hydroxybutyric acid); polyortho-esters; polyacetals; polydihydropyrans; polycyanoacrylates; polypeptides; cross-linked polypeptides; and stereoisomers, racemic mixtures, co-polymers and polymer mixtures thereof.

A particularly suitable polymer matrix comprises poly-D,L-lactide.

A suitable release profile (sink conditions, such as an aqueous pH 6 solution for diltiazem) measured in accordance with the Paddle Method of U.S. Pharmacopoeia XX at 37°C and 75 rpm for the or each drug is substantially as follows:

- a) 10-30% release within 2 hours after administration;
 - b) 30-60% release within 4 hours after administration;
 - c) 60-80% release within 8 hours after administration;
- and

- d) $\geq 80\%$ release within 24 hours after administration.

5 A further suitable release profile (sink conditions, such as simulated gastric fluid for captopril) measured in accordance with the Paddle Method of U.S. Pharmacopoeia XX at 37°C and 75 rpm for the or each drug is substantially as follows:

- a) 10-40% release within 1 hour after administration;
- b) 20-60% release within 4 hours after administration;
- c) 40-80% release within 8 hours after administration;
- and
- 10 d) $\geq 80\%$ release within 16 hours after administration.

A further suitable release profile (sink conditions, such as simulated gastric fluid for hydromorphone) measured in accordance with the Paddle Method of U.S. Pharmacopoeia XX at 37°C and 75 rpm for the or each drug is substantially as follows:

- 15 a) 10-50% release within 1 hour after administration;
- b) 40-90% release within 4 hours after administration;
- and
- c) $>90\%$ release within 8 hours after administration.

20 The effervescent formulations in accordance with the invention are suitably formulated as capsules, tablets or powders.

Thus, for convenient and effective oral effervescent administration, effective amounts of the microcapsules of the present invention can be tableted with one or more excipient(s) or encased in capsules such as gel capsules and the like.

25 It will be appreciated that the pharmaceutical formulations in accordance with the invention can be used *inter alia* in a method of

treating angina, hypertension, pain or the like by the administration of a formulation containing biologically effective amounts of at least one drug microencapsulated according to the invention to an animal, preferably a human, so as to provide and maintain clinically effective plasma levels of the drug throughout a substantial part of a 24 hour period.

The invention also provides a method for the manufacture of microcapsules as hereinbefore defined, which comprises the steps of;

- a) dissolving or dispersing a drug and a biodegradable polymer in a solvent to form a mixture;
- b) microfluidising said mixture into an external phase to form an emulsion in which the emulsion droplets have a mean diameter less than 1mm; and
- c) stirring said emulsion to form microcapsules having a size (D 50%) between about 100 nm and 900 nm.

As used herein, the term "biodegradable" as applied to polymers means synthetic or natural polymers which are degradable *in vivo* either enzymatically or non-enzymatically to produce biocompatible or non-toxic by-products which can be further metabolized or excreted *via* normal physiological pathways. For instance, a range of natural and synthetic biodegradable polymers can be used to form microparticles containing a wide variety of drugs in order to achieve prolonged drug release or drug targeting. Human serum albumin (HSA), bovine serum albumin (BSA), collagen and gelatin can be used to microencapsulate the drugs. However, the cost and uncertainty of purity of natural polymers limits their use, thus focusing attention upon synthetic biodegradable polymers in which processing conditions and availability can be controlled. Examples of synthetic biodegradable polymers are those hereinbefore specified and include the following: polylactic acid (polylactide; PLA); polyglycolic acid (polyglycolide; PGA); poly (lactic acid-co-glycolic acid) (PLGA); poly (ε-caprolactone); poly (hydroxybutyric acid); polyortho-esters; polyacetals; polydihydropyrans;

polycyanoacrylates; polypeptides; cross-linked polypeptides; and stereoisomers (i.e., D, L), racemic mixtures, co-polymers and polymer mixtures thereof. PLA is the biodegradable polymer which is most preferred.

5 The solvent evaporation method is one of the most common techniques for the production of PLA/PLGA microspheres. The first step in this method requires the formation of an oil-in-water emulsion (o/w emulsion). The polymer is dissolved in a volatile organic solvent followed by dissolution or dispersion of the drug in the polymer solution.
10 This procedure is known as forming the organic phase. The resulting polymer/drug solution is stirred in a suitable suspension medium forming a droplet suspension (o/w emulsion). The suspension medium, which should not solubilize the polymer, usually contains a dispersing agent to prevent coalescence of the droplets. The suspension medium may also
15 be referred to as the continuous phase or the external aqueous phase, the latter term being used herein.

 A modification of this solvent extraction method can be used wherein the polymer and drug are first dissolved in a water miscible organic solvent such as acetonitrile and subsequently homogenized in
20 mineral oil or light liquid paraffin to form a "w"-in-oil ("w"/o) emulsion. Another modification of this method is used, whereby a water-oil-water (w/o/w) emulsion is produced. The drug is dissolved in a small amount of water and this drug solution homogenized into a polymer/organic solvent (e.g. dichloromethane) solution. This primary water-in-oil
25 emulsion is then emulsified with the external phase, producing the w/o/w emulsion.

 Once the emulsion is formed (o/w, w/o, or w/o/w), it is subjected to solvent evaporation causing 'hardening' of the droplets (polymer solidification) and their conversion to microspheres. The emulsion is
30 stirred continually throughout the evaporation process. During the droplet hardening process, the droplets first lose their solvent by diffusion of the solvent into the external phase followed by evaporation of the solvent from the surface. The evaporation of the solvent can take

place at either atmospheric pressure or at reduced pressure. The evaporation temperature can also be varied. Solvent evaporation can be achieved in two ways: (1) interrupted evaporation in which the evaporation is stopped prior to complete elimination of the organic solvent, and the semi-solid microspheres are transferred to an emulsifier-free medium where evaporation is completed or (2) continuous evaporation in which the system is continuously agitated until all the organic solvent has completely evaporated. The solid microspheres are collected by filtration or centrifugation, washed and dried under vacuum.

Problems associated with the solvent evaporation method are agglomeration of the particles, loss of drug to the aqueous phase and the formation of drug crystals on particle surfaces. Factors affecting the quality of microspheres (i.e., drug loading, size, surface morphology), produced by the solvent evaporation method are detailed below.

In the solvent evaporation process, the organic solvent used, in addition to being able to dissolve the drug and the polymer, must be immiscible with the external phase and its boiling point must be low enough so that it will evaporate easily during the droplet hardening process. When an o/w system is used, the solvent evaporation technique works best for core materials that are insoluble in the aqueous external phase. If the core material is soluble in the external phase, it will be extracted from the microdroplets before the microsphere walls have a chance to form, resulting in lower drug loading. For instance, Bodmeier and McGinity, J. Microencap., 4:279-288 (1987) reported that water soluble drugs such as theophylline, caffeine and salicylic acid could not be entrapped by the o/w emulsion solvent evaporation method. Minimizing drug loss to the aqueous external phase can be achieved in a number of ways, such as (1) by varying the aqueous phase pH to the pH of minimal drug solubility; (2) saturating the aqueous phase with the drug; and (3) inverting the emulsification phase o/w to w/o.

The effect of using different molecular weights for a particular polymer affects the surface properties and morphology of the microspheres. For instance, high molecular weight poly-L-lactide

polymers produce larger particles that tend to aggregate due to the inherent tackiness and thermoplastic nature of the polymer. Also, highly porous microspheres are produced from high molecular weight polymers whereas microspheres produced with low molecular weight polymers
5 can be smooth and non-porous.

The diameter of the microspheres can be determined by the size of the microdroplets formed in the emulsion. The size of the microdroplets can be controlled in several ways, such as by adjusting the stirring rate, the type and the amount of emulsifier, the quantity of the aqueous phase,
10 and the configuration of the vessel and stirrer. A general increased rate of agitation results in a finer emulsion producing smaller microspheres and preventing coalescence of smaller immature microspheres.

We have found that very fine emulsion droplets can be prepared by using a Microfluidiser (Trade Mark; Microfluidics Corp.) A
15 Microfluidiser is a high pressure homogenizer capable of making very small size emulsion droplets (mean droplet diameter under 1mm). During microfluidisation, the emulsion is pumped through microchannels to an impingement area at high operating pressures. Cavitation and the accompanying shear and impact is responsible for the
20 particle size reduction within the "interaction chamber".

Drug release from biodegradable systems may range from purely diffusion-controlled dissolution from a matrix system in cases in which the polymer has a slow degradation rate and the drug molecule is small, to degradation-controlled release when the drug molecule is large and its
25 permeability in the polymer is low. With the more rapidly degrading polymers, drug release can occur through a combination of diffusion and degradation of the polymer. The possible mechanisms of drug release from biodegradable microsphere systems may be summarized as follows; (1) drug which is loosely bound to or embedded in the microsphere
30 surface is released initially resulting in a "burst effect"; (2) depending on microsphere structure, drug may be released through the microsphere pores; (3) drug may diffuse through the polymer membrane depending on the solubility of the drug in the polymer membrane and the intrinsic

properties of the polymer; (4) the drug may diffuse through the water swollen polymer barrier depending on the hydrophilicity and in turn the molecular weight of the polymer; and (5) erosion and hydrolysis of the polymer chains causes pore formation in the microsphere structure and hence affects the rate of drug release. All these possible mechanisms may together play a part in the release process depending on the morphology of the microsphere systems (which in turn is affected by manufacturing techniques), polymer composition and physiochemical properties of the drug.

Drug release from microsphere systems is dependent on the diffusivity of the drug through the polymer barrier, the solubility of the drug in the bulk phase, the size of the drug molecule and its distribution throughout the microsphere matrix. The nature of the polymer plays a major role in determining release characteristics, in particular the molecular weight of the polymer. For instance, the effect of polymer molecular weight on *in vitro* release of chlorpromazine from chlorpromazine loaded poly-DL-lactide microspheres using poly-DL-lactide in a molecular weight range from 11,000 to 21,000, in pH 7.0 aqueous phosphate buffer has been studied. Increased polymer molecular weight increased the time required for 50% release. Microspheres produced from the higher molecular weight polymers exhibited a lag time of ≥ 24 hours at which time the release rate increased rapidly to approximately $\pm 40\%$ release.

Furthermore, two of the most important microsphere characteristics that affect drug release are drug loading and microsphere size.

Early theories which have been put forward to describe the dissolution process from matrix systems were very often based on Fick's laws of diffusion. Fick's first law of diffusion states that the flux (J) of a compound across a unit area of a predetermined reference plane is proportional to the concentration differential across that plane, the proportionality constant being the diffusivity (D). Based on Fick's first law of diffusion, Higuchi developed an equation for release of solid drug

from an ointment base and later applied it to the diffusion of solid drugs dispersed in homogenous and granular matrix dosage systems as follows:

$$Q = (D(2A - C_s) C_s T)^{-1/2} \quad (\text{Equation 1})$$

where

- 5 D = the diffusivity of the drug in the matrix;
- A = the total amount of drug per unit volume of matrix;
- C_s = the solubility of drug in the polymer matrix;
- Q = amount of drug per unit area of matrix; and
- T = time.

- 10 Later, using the same diffusion principle as Higuchi, Cobby *et al.* presented equations describing the release of drug from matrix tablets having either a spherical, cylindrical or biconvex shape. In each case, the three dimensional equation had the cubic form:

$$F = G_1(KT) - G_2(KT)^2 + G_3(KT)^3 \quad (\text{Equation 2})$$

- 15 where

- F = the fraction of drug released;
- T = the elapsed time;
- K = the release rate constant;
- $G_1 - G_3$ are shape factors.

- 20 For a spherical shape G_1 and $G_2=3$ and $G_3 = 1$.

 The fundamental parameters of the release rate constant are described by

$$K = 1/A \cdot r \div D C_s (2A - eC_s)e/t.$$

where r = initial tablet radius;

e = porosity; and

t = tortuosity.

5 The Prout-Tomkins' equation has been applied to the autocatalytic decomposition of solid, i.e., the drug acting as a marker of polymer degradation:

$$\ln (c/1-c) = K \times t + c \quad \text{(Equation 3)}$$

where c = the fraction of drug released at time t ;

10 K = the rate constant; and

$c = K \times t_{\max}$ (t_{\max} is the time taken for 50% of the drug to be released).

15 The release of diltiazem base from DL-PGLA microspheres in phosphate buffer pH 7.4 has been fitted to the Prout-Tomkins' equation (Fitzgerald *et al.*, Polymeric Delivery Systems, Properties and Applications, Chap. 23 (ACS Symposium Series 520) (1992)). The systems studied had drug loadings of 4.45%, 10.06% and 20.22 % and were in the <125 μ m size range. In all cases, the fits obtained were good, suggesting that release from these systems was dependent on
20 polymer degradation and dissolution.

Various methods can be used to obtain microcapsules as follow:

Drug Dissolved in Solvent Method (Method A)

This method is similar to the oil-in-water (o/w) emulsion solvent evaporation techniques. The drug and polymer are dissolved in a suitable solvent (such as dichloromethane) to form the oil phase. An aqueous 0.27% w/v PVA solution is suitably used as the external phase. 5 The oil phase is emulsified into the external phase to form a droplet suspension for example by one of the following methods:

- (i) Using an IKA Ultra Turrax T25 (Trade Mark) for two minutes at 8,000, 9,500, 13,500 or 24,000 rpm;
- 10 (ii) Using an M120E Microfluidiser (Microfluidics Corp.) at 10,000 psi for a specified number of cycles.

The resulting emulsion can be stirred for example with an IKA RW25 motor and 4-blade stirrer at 1,400 rpm for one hour causing the polymer droplets to lose their solvent, initially by diffusion of the solvent into the aqueous external phase and subsequently by evaporation. In this 15 way, the polymer droplets are converted to the corresponding solid microspheres.

The microspheres are suitably collected by centrifugation (Heraeus Sepatech Biofuge 28RS) using a HFA 13.5 rotor at 13,000 rpm for 15 minutes and then dried in a vacuum oven (Gallenkamp) at 1,000 20 mbar for 24 hours. The microspheres are stored in airtight containers at room temperature.

Dispersion Method (Method B)

The oil phase is formed by dispersing the drug in the polymer/solvent solution using sonication. The oil phase is emulsified 25 into the external aqueous phase by Method A (i) or (ii). This step is followed by solvent evaporation, collection, drying and storage as outlined in Method A. Final microsphere size is dependent on drug crystal size. This limitation can be overcome by dissolving the drug in a co-solvent as outlined in Method C below.

30 Co-Solvent Method (Method C).

The drug is first dissolved in the minimum amount of a suitable solvent (such as methanol). The polymer/solvent solution is then added to the drug solution and sonicated to form the oil phase. The oil phase is emulsified into the external aqueous phase by Method A (i) or (ii). This step is followed by solvent evaporation, collection, drying and storage as outlined in Method A. As described below, diltiazem HCl was entrapped using Method C in microspheres formed from PLA with a molecular weight average of 109,000 (PLA 109K). The formulation used for a 10% w/w starting loading was as follows:

10	PLA 109K : Dichloromethane	0.9 g : 10 ml
	Diltiazem HCl : Methanol	0.1 g : 0.5 ml
	Dichloromethane : 0.27% PVA	1 ml : 10 ml

For all methods when entrapping diltiazem, the PVA solution is suitably buffered to pH 10.0 (pH of least solubility of diltiazem in an aqueous solution) suitably using a carbonate buffer prepared as follows:

NaHCO ₃	3.915 g/l
Na ₂ CO ₃	5.660 g/l

Double Emulsion Method (Method D)

This method is an adaptation of a (water-in-oil)-in-water (w/o/w) solvent evaporation technique which has previously been found to be successful in entrapping hydrophilic agents in polylactide-co-glycolide microparticles (Ogawa *et al.*, Chem. Pharm Bull., 36:1502-1507 (1988)). In a modification of this method carried out by us the drug was dissolved in a 5% w/v gelatin solution (internal aqueous phase). The polymer/dichloromethane solution was added to the drug solution and emulsified at 24,000 rpm for one minute using as IKA Ultra Turrax T10. The resulting w/o emulsion was then emulsified into the 0.27% w/v PVA external aqueous phase by one of the following methods to produce the w/o/w emulsions:

- (i) Using an IKA Ultra Turrax T18 at 8,000 rpm for two minutes;
- (ii) Using an M120E Microfluidiser (Microfluidics Corp.) at 10,000 psi for a specified number of cycles.

5 The droplet hardening process was carried out by stirring the w/o/w emulsion at 1,400 rpm for 30 minutes - 1 hour (depending on the amount of solvent used) with an IKA RW25 and 4-blade stirrer. The microspheres were collected, dried and stored as outlined for Method A. For diltiazem HCl, the drug: gelatin solution ratio was 0.1 g : 0.1 ml; the
10 polymer : solvent ratio was PLA 109K 1 g : 4 ml; and the external phase was 100 ml per 2 g total batch weight.

***In vitro* Dissolution Studies**

Dissolution studies herein were carried out in the following dissolution media:

- 15 (i) Isotonic phosphate buffer pH 7.4
- | | |
|--|-----------|
| NaCl | 4.4 g/l |
| NaH ₂ PO ₄ (anhydrous) | 1.615 g/l |
| Na ₂ HPO ₄ (anhydrous) | 7.571 g/l |
- 20 (ii) Simulated gastrointestinal fluid (SGF) pH 1.2
- | | |
|------------------|----------|
| NaCl | 2.0 g/l |
| Concentrated HCl | 7.0 ml/l |

Stoppered dissolution flasks were filled with a measured volume of the desired dissolution medium and placed in a water bath at a constant temperature of 37°C. After the solution had reached equilibrium, a desired amount of sample was added into the flask. The sample weight was predetermined to prevent the drug concentration in the medium from exceeding 10% of its solubility and thus maintain sink conditions. The samples were either dispersed in the dissolution media, or, if the samples were in the submicron size range, they were contained in a 14 cm length of Visking tubing tied at both ends. The dissolution flasks were shaken at 60 rpm.

Brief Description of the Drawings

Fig. 1 shows the release profiles in phosphate buffer pH 7.4 of diltiazem HCl from 10% w/w loaded PLA 109K microsphere systems prepared by Method C, D₁ (D 50% of 12.56 mm), D₂ (D 50% of 5.76 mm); D₃ (D 50% of 2.86 mm); and D₄ (D 50% of 1.41 mm);

Fig. 2 shows the release profiles in simulated gastric fluid (SGF) pH 1.2 of diltiazem HCl from 10% w/w loaded PLA 109K microsphere systems prepared by Method C, D₁ (D 50% of 12.56 mm), D₂ (D 50% of 5.76 mm); D₃ (D 50% of 2.86 mm); and D₄ (D 50% of 1.41 mm);

Fig. 3 shows release profiles in phosphate buffer pH 7.4 of diltiazem base from PLA 109K microsphere systems prepared by Method A with the Ultra Turrax (Db₂-Db₅) 10%, 20%, 30% and 50% w/w, respectively;

Fig. 4 shows release profiles in SGF pH 1.2 of diltiazem base from PLA 109K microsphere systems prepared by Method A with the Ultra Turrax (Db₂-Db₅, 10-50% w/w respectively); and

Figs. 5, 6 and 7 show, respectively, release from 20%, 30% and 50% diltiazem base loaded PLA 109K nanospheres at pH 1.2, pH 6.0 and pH 7.4 (as prepared in Example 8).

5 Fig. 8 shows the diltiazem plasma levels over a period of 36 hours in humans following administration of 20%, 30%, and 50% diltiazem base loaded PLA 109K nanospheres (reference is Cardizem CD).

Fig. 9 shows release from hydromorphone loaded microcapsules encased in gel capsules into simulated gastric fluid (0.01 M HCl).

10 Fig. 10 shows release from nifedipine loaded microcapsules (50% loaded R203 and 50% loaded RG 504 microspheres) and nifedipine loaded microcapsules that were mixed with lactose and tableted prior to dissolution (30% loaded R203 and 50% loaded RG 504 microspheres); Nifed retard is shown as a control.

15 Diltiazem HCl was converted to the base form when required herein by preparing a saturated diltiazem HCl aqueous solution and adding an excess of 1 M NaOH until precipitation occurred. Recovery of the diltiazem base was followed by drying in a desiccator under vacuum for two days.

20 Modes for Carrying Out the Invention

The invention will be further illustrated by the following Examples.

EXAMPLE 1

25 An attempt was made to prepare diltiazem loaded PLA microspheres using Method A, a method involving as described above the evaporation of solvent from an o/w emulsion, the oil phase being formed by dissolving the drug and polymer in dichloromethane. This

method was not suitable as diltiazem HCl did not dissolve in dichloromethane.

EXAMPLE 2

Attempts to prepare diltiazem HCl loaded PLA microspheres by Method B were unsuccessful. Method B also involved the evaporation of solvent from an o/w emulsion, the oil phase being formed by dispersing the drug in the polymer/solvent solution using sonication. Diltiazem HCl crystals when observed under the light microscope were seen to be too large and irregular in shape for entrapment by this method. This finding was substantiated by particle size analysis: diltiazem HCl had a D 10% of 19.01 mm, D 50% of 41.83 mm and a D 90% of 72.61 mm.

EXAMPLE 3

Diltiazem HCl loaded PLA 109K microspheres were prepared using Method C, whereby the drug was first dissolved in the minimum amount of a suitable solvent (methanol). The polymer/solvent solution was then added to the drug solution and sonicated to form the oil phase. The oil phase was emulsified into the external aqueous phase (buffered to pH 10.0) using the 1KA Ultra Turrax at four different homogenization speeds. All the systems prepared by Method C had a starting loading of 10% w/w. Microsphere system D₁ was prepared at the lowest homogenization speed setting on the Ultra Turrax, i.e., 8,000 rpm., the microspheres produced had a drug entrapment efficiency of 86.0%. The homogenization was subsequently increased to 9,500, 13,500 and 24,000 rpm to produce microsphere systems D₂, D₃ and D₄ having drug entrapment efficiencies of 98.7%, 89.4% and 63.8% respectively, as shown in Table 1.

TABLE 1							
Lot No.	Speed of Homogenization Ultra Turrax rpm	Entrapment efficiency %	Yield %	D 10% mm	D 50% mm	D 90% mm	Span
D ₁	8000	86.0	80.5	3.76	12.56	67.61	4.97
D ₂	9500	98.7	80.0	2.29	5.76	16.39	2.44
D ₃	13500	89.4	86.0	0.67	2.86	5.61	1.73
D ₄	24000	63.8	79.5	0.65	1.41	3.59	2.09

There was a marked decrease in the size of the microspheres with increasing homogenization speed. The D 50%, of the microspheres decreased from 12.85 mm to 1.41 mm as the homogenization speed was increased from 8,000 rpm to 24,000 rpm. There was a corresponding decrease in the D 90% from 67.61 mm to 3.59 mm and in the D 10% from 3.76 mm to 0.65 mm. This relationship was not linear when plotted on a log-log scale.

10

The entrapment efficiency of the microspheres was found to be dependent on the homogenization speed used. With increasing homogenization speed, there was an initial slight increase followed by a drop in efficiency with further decrease in size. This may be due to the fact that the smaller particles have a larger surface area/volume ratio resulting in greater drug loss to the aqueous external phase during processing. Percentage entrapment efficiency ranged from 63.8% to 98.7%. It was not possible to exceed 10% w/w starting loading as the amount of diltiazem needed for a starting loading greater than 10% w/w would not dissolve in 0.5 ml of methanol and in this formulation the ratio of methanol to dichloromethane should not exceed 0.5 ml to 10 ml.

15

SEM photomicrographs of all the microsphere systems prepared by Method C show smooth, spherical microspheres. Microspheres produced with the lowest homogenization speed 8,000 rpm were large with a D 50% value of 12.56 mm and had a wide size distribution, as indicated by the span value of 4.97. In comparison, microspheres

20

25

produced with the highest homogenization speed, 24,000 rpm, were smaller with a D 50% value of 1.41 mm and had a narrower size distribution, as indicated by the span value of 2.09. Microspheres produced at 9,500 and 13,000 rpm were also more uniform in size than D₁ with span values of 2.44 and 1.73, respectively.

The diltiazem HCl loaded PLA 109K microspheres prepared by Method C were analyzed by differential scanning calorimetry (DSC). The diltiazem HCl used was crystalline having a thermal event at 217°C. PLA 109K showed a thermal event at 65.6°C. DSC thermograms of the microspheres prepared by Method C showed no detectable crystalline diltiazem HCl. Physical mixtures containing 10% w/w and 5% w/w diltiazem HCl in PLA 109K had thermal events at 215.2°C, 65.5°C and 214.0°C, 63.9°C, respectively. A DSC scan of a 3% diltiazem in PLA 109K physical mixture showed a thermal event at 65.9°C only, indicating that 3-5% is the limit of detection for a diltiazem HCl/PLA 109K system.

X-ray diffraction patterns show the absence of crystalline diltiazem HCl in the systems prepared by Method C, indicating that diltiazem HCl is present in an amorphous or solubilized state.

EXAMPLE 4

Diltiazem HCl loaded PLA 109K microsphere systems were prepared by Method D, a method involving the evaporation of solvent from a double emulsion (w/o/w emulsion). The drug was initially dissolved in a 5% w/v gelatin solution to form the internal aqueous phase. The polymer/dichloromethane solution was added to the drug solution and emulsified using the Ultra Turrax at 24,000 rpm for one minute. The resulting w/o emulsion was then emulsified into the external aqueous, phase (buffered to pH 10.0) using the Ultra Turrax at 8,000 rpm for two minutes. Microspheres with a starting loading of 10% w/w (D₅) were produced and had an entrapment efficiency of 96.8%. The starting loading was subsequently increased to 20% w/w (D₆); the microspheres produced had an entrapment efficiency of 85.5%, finally,

microspheres with a starting loading of 30% w/w (D7) had an entrapment efficiency of 71.5%. As the starting loading was increased from 10% w/w to 30% w/w the entrapment efficiency decreased from 96.8% to 71.5%.

5

Using Method D, it was possible to prepare microspheres with up to 30% w/w starting loading, whereas with Method C it was not possible to exceed a starting loading of 10% w/w due to the limited solubility of the diltiazem HCl in the co-solvent (methanol). For Method D, in order to control the viscosity of the primary emulsion, the drug to gelatin ratio was kept at 0.1 g : 0.1 ml. Therefore, it was not possible to exceed a starting loading of 30% w/w as the diltiazem HCl necessary to achieve a drug loading of greater than 30% w/w would not dissolve in the gelatin solution.

15

Method D resulted in batches with lower percentage yield (54.0 - 63.5%) than those obtained using Method C (79.5 - 86.0%). This may be due to greater loss of product to vessel surfaces and homogenizer heads etc. during the two step process involved in Method D.

Entrapment efficiency results shown in Table 2, for Methods C and D were comparable, ranging from 63.8-98.7% for Method C to 71.5-96.8% for Method D.

TABLE 2								
Lot No.	Starting Loading % w/w	Actual Loading % w/w	Entrapment efficiency %	Yield %	D 10% mm	D 50% mm	D 90% mm	Span
5	5 10	9.68	96.8	60.0	1.37	5.39	15.81	2.65
6	D 20	17.10	85.5	54.0	3.34	15.95	42.97	2.60
7	D 30	21.46	71.5	63.5	2.88	9.43	60.65	4.39

25

SEM photomicrographs of the systems produced by Method D showed the particles to be spherical, however the surfaces of these

particles showed some irregularities. System D7, 30% w/w starting loading had some drug crystals present between the microspheres and on the microsphere surfaces. Particle size distribution plots for microsphere system D5, showed bimodal distribution of particles whereas particle size distribution plots for microsphere system D7 show multimodal distribution, which may be due to the presence of drug crystals, polymer debris or very small particles. Microsphere size was found to increase with increased drug loading. Microsphere system D5 10% w/w starting loading, had a D10% of 1.37 mm and a D90% of 15.81 mm compared to a D 10% of 2.99 mm and a D90% of 60.65 mm for (D5), 30% w/w starting loading.

EXAMPLE 5

In-Vitro Release Studies: The effect of particle size on the release of diltiazem HCl from 10% loaded PLA 109K microspheres

Prior to carrying out *in vitro* release studies, the saturated solubility of diltiazem HCl was measured in order to establish sink conditions. Diltiazem HCl was found to have Cs values of 2.39 g/l in phosphate buffer pH 7.4, and greater than 1 g/ml in pH 1.2. The microsphere systems studied had a diltiazem HCl loading of 10% w/w and were prepared by Method C.

Release profiles of diltiazem HCl from PLA 109K microspheres obtained in isotonic phosphate buffer pH 7.4 showed release to be retarded when compared with release of pure diltiazem. HCl. Secondly, release was found to be related to the size of the particles. For a given mass of particles, the larger size microsphere released diltiazem at a slower rate than the smaller size particles. The release profiles are in rank order from the largest microspheres, D1 produced at 8,000 rpm with a D50% of 12,56 mm, to D4 produced at 24,000 rpm with a D50% of 1.41 mm (Fig. 1). Release profiles of diltiazem HCl from PLA 109 K microspheres obtained in SGF pH 1.2 also showed release to be retarded when compared with release of pure diltiazem HCl. In SGF, there was a high initial "burst" effect, smaller particles released up to 60% of drug in

the first 24 hours. This was probably due to the solubility of the drug being greater in simulated gastric fluid (SGF) than in phosphate buffer. The release profiles of the larger microsphere systems D₁ (D50% of 12.56 mm, to D₄ produced at 24,000 rpm with a D50% of 1.41 μ m.

5 Release profiles of diltiazem HCl from PLA 109K microspheres obtained in SGF pH 1.2 also showed release to be retarded when compared with release of pure diltiazem HCl. In SGF, there was a high initial "burst" effect, smaller particles released up to 60% of drug in the first 24 hours. This was probably due to the solubility of the drug being
10 greater in SGF than in phosphate buffer. The release profiles of the larger microsphere system D₁ (D50% of 12.56 mm) and D₂ (D50% of 5.76 mm) were similar: drug release from these systems was very slow. The smaller systems D₃ (D50% of 2.86 mm) and D₄ (D50% of 1.41 mm) also had similar release profiles and released diltiazem at a faster
15 rate (Fig. 2).

 Release profiles were fitted to Equation 2, which describes the release of drug from a spherical matrix. The rate constant K is defined by the Higuchi type equation. The best estimates of K by non-linear least square and values of correlation coefficient are given below in
20 Table 3. The fits were considered relatively good in phosphate buffer pH 7.4, as measured by the correlation coefficients. Release appeared to be primarily diffusion controlled.

TABLE 3			
Lot No.	D 50% mm	K	correlation
D ₁	12.56	0.00382	0.099714
D ₂	4.76	0.01008	0.97049
D ₃	2.86	0.01782	0.99170
D ₄	1.41	0.29023	0.99608

The correlation coefficients of the release data in pH 1.2 were poor. When the release data for the first five hours of diltiazem release in SGF was fitted to Equation 2, the correlation coefficients were much improved, indicating that release at the earlier time points was diffusion controlled. Values of K were found to be inversely proportional to particle size. As the D 50% decreased from 12.85 mm (D₁) to 1.41 mm (D₄), the value of K increased from 0.00382 to 0.29023 in phosphate buffer, and from 0.00783 to 0.03586 for release in the first five hours in SGF.

Release studies were stopped after 500 hours. The microspheres were collected, dried and assayed after dissolution in SGF. The drug content of the microspheres was as follows D₁:6.70% w/w; D₂: 7.42% w/w; D₃3.06% w/w; D₄: 2.35% w/w, i.e., the drug had not degraded in the microspheres. Subsequent release from these systems may have been controlled by degradation of the polymer.

EXAMPLE 6

Diltiazem base is soluble in dichloromethane, therefore Method A, a method involving the evaporation of solvent from and o/w emulsion, the oil phase being formed by dissolving the drug and polymer in

dichloromethane was suitable for the preparation of diltiazem base loaded PLA 109K microspheres. All batches were prepared using a 1:11 ratio of PLA 109K dichloromethane. Microspheres with a starting loading of 10% w/w up to 80% w/w were prepared. The oil phase was homogenized into the external aqueous phase (buffered to pH 10.0) using the 1KA Ultra Turrax at 8,000 rpm for all systems except Db₁. As shown in Table 4, entrapment efficiencies in the range 61.85 - 88.5% were achieved. Product yield was high at all loadings, ranging from 83.0% to 97.0%.

10

TABLE 4								
Lot No.	Starting Loading % w/w	Actual Loading % w/w	Entrapment efficiency %	Yield %	D 10% mm	D 50% mm	D 90% mm	Span
Db ₁	10	6.99	69.9	84.5	2.62	18.58	76.7 2	4.00
Db ₂	10	7.63	76.3	83.0	1.21	3.27	7.17	1.82
Db ₃	20	16.61	83.04	97.0	1.51	4.02	7.25	1.43
Db ₄	30	18.53	61.8	87.5	1.19	3.45	6.10	1.42
Db ₅	50	36.27	72.53	88.0	1.27	4.02	7.72	1.61
Db ₆	50	33.43	66.86	95.5	1.69	5.86	8.90	1.23
Db ₇	80	70.78	88.5	86.3	2.75	13.07	27.0 3	1.23
Db ₈	90	not possible	-	-	-	-	-	-

Using a 10% w/w starting loading, microsphere system Db₂ was prepared using the 1KA Ultra Turrax at the lowest speed setting of 8,000 rpm to emulsify the oil phase into the external aqueous phase. Microspheres with a D50% of 3.27 mm were produced (diltiazem HCl

15

loaded microspheres prepared at the same homogenization speed using Method C had a larger D50% of 12.56 mm).

Microsphere system Db₁ was prepared using a T25 stirrer at a much lower speed setting of 1,400 rpm to emulsify the oil phase into the external aqueous phase. The microspheres were larger as expected with a D50% of 18.58 mm. The microspheres prepared with the IKA Ultra Turrax had a higher entrapment efficiency than those prepared with the T25 stirrer. Since it was established that the IKA Ultra Turrax could efficiently produce small particles at 8,000 rpm using Method A, this speed setting was used for subsequent batches Db₃ -Db₇.

Diltiazem base is less soluble in water than diltiazem HCl, therefore significantly higher drug loading could be achieved (up to 80% w/w starting loading) as there was very little loss of drug to the external aqueous phase. It was not possible to exceed a starting loading of 80% w/w as the amount of diltiazem base necessary to achieve greater loading would not dissolve in the given amount of dichloromethane. Using Method A with the Ultra Turrax, microspheres with entrapment efficiencies in the range 61.8-88.5% were produced. Entrapment efficiency was independent of starting loading. Product yield ranged from 83.0% to 97.0% and was also independent of starting loading.

Diltiazem base loaded PLA 109K microsphere systems prepared by Method A at drug loadings of 10, 20, 50 and 80% w/w were analyzed by DSC. The diltiazem base starting material used had a thermal event at 105°C. PLA 109K had a thermal event at 65.6°C. Physical mixtures containing 10% and 30% w/w diltiazem base had thermal events at 64.8°C, 104.4°C, 64.6°C and 104.7°C, respectively. The limit of detection for a diltiazem base/PLA 109K system is 10% w/w. DSC thermograms of systems Db₂, Db₃ and Db₅ showed no detectable crystalline diltiazem base, whereas Db₇ had a thermal event at 105.4°C, indicating the presence of crystalline diltiazem base.

SEM photomicrographs of diltiazem base loaded PLA 109K systems prepared by Method A using the Ultra Turrax showed spherical

particles. The surfaces of the particles were smooth. However, at 50% w/w loading there was some debris on the microsphere surfaces and in between the microspheres; this may be polymer or drug crystals. At 80% w/w loading there was a considerable amount of drug crystals present.

With the exception of Db7, particle size results of all microsphere systems prepared with the Ultra Turrax were very reproducible, with D10% ranging from 1.19-1.69 mm, D50% ranging from 3.27-5.86 mm and D90% ranging from 6.10-8.90 mm. Microspheres of system Db7 were larger with a D 50% of 13.07 mm. Microsphere systems prepared with the Ultra Turrax (Db2 - Db6) were also reasonably uniform in size with span values ranging from 1.23-1.82. In contrast, microspheres of microsphere system Db1, prepared at 1,400 rpm with the T25 stirrer, were much larger (D50% of 18.58 mm) and had a wider size distribution, as indicated by a span value of 4.00 and particle size distribution plots.

EXAMPLE 7

In-vitro release studies: The effect of drug loading on the release of diltiazem base from PLA 109K microspheres

Prior to carrying out *in vitro* release studies, the saturated solubility of diltiazem base was measured in order to establish sink conditions. Diltiazem base was found to have Cs values of 227.47 g/l in SGF pH 1.2 and 1.06 g/l in phosphate buffer pH 7.4. The microsphere systems studied had diltiazem base starting loadings of 10% w/w, 20% w/w, 30% w/w, and 50% w/w, D 50% of 3.27 mm, 3.45 mm, 4.02 mm, respectively, and were prepared by Method A using the Ultra Turrax.

Release profiles of diltiazem base from PLA 109K microspheres in isotonic phosphate buffer pH 7.4 showed release to be dependent on percentage drug loading. Microspheres at the lower drug loading of 10% w/w released diltiazem base at a slower rate. The release profiles were in rank order the lowest drug loading 10% w/w to the highest drug loading 50% w/w. There was very little difference in the release profiles

of microspheres at 30% and 50% w/w (Fig. 3). Release profiles of diltiazem base from PLA 109K microspheres in SGF pH 1.2 also showed release to be dependent on percentage drug loading. The release profiles were again in rank order (Fig. 4). There was a notable difference
5 between the release profiles of microspheres at 30% and 50% w/w loading. Microspheres at 50% w/w loading released diltiazem base at a very fast rate. Diltiazem base had a high solubility in SFG. Additionally, at high drug loadings there may be drug at or near to the surface of the microspheres; this may explain the very fast release rate
10 from microspheres at 50% w/w loading. The release profiles in phosphate buffer and in SFG were fitted to Equation 2.

The fits may be considered relatively good, as measured by the correlation coefficients. Release in phosphate buffer appeared to be primarily diffusion controlled. Release in SGF from microspheres with
15 high drug loading also appeared to be primarily diffusion controlled. At lower drug loadings (20% w/w), release was diffusion controlled at the earlier time points. Later release may have been controlled by a combination of diffusion and polymer degradation as indicated by SEM photomicrographs after dissolution. Values of K were found to be
20 proportional to A, the mass of drug initially present. As the starting drug loading increased from 10% w/w (Db₂) to 50% w/w (Db₅), the value of K increased from 0.00378 to 0.02130 in phosphate buffer and from 0.00229 to 0.22015 in SGF.

SEM photomicrographs taken after dissolution of microsphere
25 system Db₃, 20% w/w drug loading, showed complete degradation of the microspheres in both phosphate buffer and SGF suggesting that release at later time points was controlled by a combination of diffusion of the drug into the dissolution medium and degradation of the polymer. Microspheres at 50% w/w drug loading, Db₅ remained intact in SGF,
30 suggesting that at higher drug loading release in SGF was totally diffusion dependent due to the high solubility of the drug in SGF. These microspheres were degraded in phosphate buffer as release in phosphate buffer was slower due to the reduced solubility of the drug and the faster degradation of the polymer at pH 7.4.

EXAMPLE 8

Diltiazem base loaded PLA 109K microspheres were prepared by Method A using the Microfluidiser (Trade Mark), high pressure homogenizer, to homogenize the oil phase into the external aqueous phase (buffered to pH 10.0). The Microfluidiser was operated at 10,000 psi for one cycle. All batches were prepared using a 1.11 ratio of PLA 109K : dichloromethane. As shown in Table 5, microspheres with a starting loading of 10% w/w were prepared and an entrapment efficiency of 53.7% was achieved. Subsequent systems with starting loadings of 20%, 30% and 50% w/w were prepared. Entrapment efficiencies of 68.1%, 65.2% and 84.5% respectively were achieved and product yields in the range of 56.0% to 67.5% were obtained.

TABLE 5

Lot No.	Starting loading % w/w	Actual loading % w/w	Entrapment efficiency %	% yield	Z average nm
Db9	10	5.37	53.7	67.0	302.5
Db10	20	13.61	68.1	60.0	294.0
Db11	30	19.56	65.2	67.5	307.5
Db12	50	42.08	84.2	56.0	310.0

Whether the Ultra Turrax or the Microfluidiser was used for homogenization, the range of entrapment efficiency was not affected; the

Ultra Turrax produced batches with entrapment efficiencies in the range of 61.8-88.5% while the Microfluidiser produced batches with entrapment efficiencies in the range of 53.7-84.2%. However, the percentage yields were lower when the Microfluidiser was used for homogenization. That is, yields of 56.0-67.0% were achieved with the Microfluidiser compared to 83.0-97.0% with the Ultra Turrax. This may be due to the difficulty in fully recovering product from the Microfluidiser.

Microsphere systems prepared by Method A using the Microfluidiser, Db9-Db12, had Z average mean size values in the range of 294-310 nm, illustrating that the Microfluidiser is a very effective homogenizer capable of producing very fine emulsion droplets. The particle size was independent of drug loading. Systems with a 10% w/w loading had a Z average mean size value of 302.5 nm while systems with 50% w/w loading had a Z average mean size value of 310.0 nm. The particles produced by this method had smooth surfaces and were spherical in shape. These systems were also uniform in size as seen in SEM photomicrographs of the systems.

EXAMPLE 9

The effect of drug loading and pH on the *in vitro* release of diltiazem base from PLA 109 K microspheres prepared with the Microfluidiser

The microsphere systems studied had diltiazem base starting loadings of 10% w/w, 20% w/w, 30% w/w and 50% w/w, Z average mean sizes of diameter (D50%) 302.5 nm, 294.0 nm, 307.5 nm, and 310.0 nm, respectively, and were prepared by Method A using the Microfluidiser. Release profiles of diltiazem base from PLA 109K microspheres, obtained in isotonic phosphate buffer pH 7.4, showed release to be dependent on drug loading at the earlier time points (i.e., from 1-25 hours). Release profiles were superimposable over the 200 hour study period, the effect of drug loading on release was not seen. In contrast, release of diltiazem base from PLA 109K microspheres in SGF

was found to be dependent on drug loading. Release profiles were in rank order, microspheres with 10% w/w starting loading released diltiazem base at the slowest rate, microspheres with 50% w/w starting loading released diltiazem base almost immediately. Figs. 5-7 show release from 20%, 30% and 50%, respectively, diltiazem base loaded PLA 109K nanospheres at pH 1.2, pH 6.0 and pH 7.4 (prepared according to Example 8). Because of the delivery characteristics of these microcapsules over a 24 hour period, these formulations are appropriate for once-daily administration of diltiazem.

In both media, release of diltiazem base from microsphere systems prepared with the Microfluidiser was much faster when compared to release from microsphere systems prepared with the Ultra Turrax. At 168 hours, Db9 microspheres (10% w/w loading, prepared with the Microfluidiser) had release 100% diltiazem base in phosphate buffer pH 7.4 compared to only 16.06% from Db2 (10% w/w loading, prepared with the Ultra Turrax).

Release profiles were fitted to Equation 2. The best estimates of K by non-linear least squares and values of correlation coefficient are given below. The fits may be considered relatively good as measured by the correlation coefficients. Release appeared to be diffusion controlled.

TABLE 6: The best estimates of K by non-linear least squares and values of correlation coefficient for diltiazem base release in phosphate buffer pH 7.4			
Lot No.	Drug loading % w/w	K	correlation
Db9	5.37	0.03572	0.98990
Db10	13.61	0.04064	0.99201
Db11	19.56	0.04234	0.99107
Db12	42.08	0.04358	0.99816

The correlation coefficients of the release data in SGF pH 1.2 were poor when plotted over the entire course of the release study, particularly at the lower drug loading of 10% and 20% w/w. The fits were considered relatively good for diltiazem release at the higher drug loading of 50% w/w, indicating that release was diffusion controlled. When the release data for the first five hours of diltiazem release in SGF was fitted to Equation 2, the correlation coefficients were much improved, indicating that release at the earlier time points was diffusion controlled and release was subsequently controlled by degradation of the polymer. This may be due to the fact that at the lower drug loadings there was less drug at or near the surface of the microspheres; therefore, there was less drug accessible to the dissolution medium. Polymer degradation must have occurred in order to allow drug release. Values of K were found to be proportional to drug loading. As the loading increased from 5.37% w/w (Db₉) to 42.08% w/w (Db₁₂), the value of K increased from 0.03572 to 0.04358 in phosphate buffer and from 0.07678 to 0.44293 for release in the first five hours in SGF.

TABLE 7: The best estimates of K by non-linear least square and values of correlation coefficient for diltiazem base release in SGF pH 1.2

Lot No.	Drug loading % w/w	Release in SGF - Hours 0-200 K correlation		Release in SGF - Hours 1-5 K correlation	
Db ₉	5.37	0.03620	0.82297	0.07678	0.98313
Db ₁₀	13.61	0.08651	0.90619	0.12027	0.94174
Db ₁₁	19.56	0.17499	0.93772	0.18784	0.95852
Db ₁₂	42.08	0.44293	0.96204	0.44293	0.96204

EXAMPLE 10

Diltiazem *in-vivo* studies

5 Diltiazem nanoparticles were prepared in accordance with Examples 8 and 9 at starting drug loading of 20%, 30% and 50% for enclosure into a capsule (e.g., gel capsule). Diltiazem HCl (USP Grade) was used as the active ingredient. Poly-D, L-lactide (R206 Boehringer Ingelheim), molecular weight 109,000, inherent viscosity of 1.0, was used as the biodegradable polymer. The potency of the capsules was
10 determined using high performance liquid chromatography in accordance with the method detailed in the USP.

Release characteristics of the test product were established prior to the study in accordance with the Paddle Method of U.S. Pharmacopoeia XX at 37°C and 75 rpm. The test product was shown to exhibit the
15 following *in vitro* release profile:

	Time (hr)	% release
	2	10-30
	4	30-60
	8	60-80
20	24	≥80

180 mg of the three test products were administered to human volunteers. Cardizem CD 180 mg (Trade Mark, Marion Merrell Dow) was used as the reference in this study. Microfluidised microcapsules/nanoparticles, as prepared in accordance with Example 8,
25 were used in preference, since the Z average mean diameter ranges (294-310 nm) and starting loading (10% to 50% w/w) provide characteristics which are most preferable for use in these preparations. The diltiazem

plasma levels were measured over a period of 36 hours as shown in Fig. 8. Both the 20% and 30% starting loading preparations showed desirable controlled release and bioavailability characteristics over at least a 24 hour period of time.

5

EXAMPLE 11

Captopril *in vivo* Studies

Captopril nanoparticle capsules are prepared using a spray drying technique. Captopril (USP grade) is used as the active ingredient. Poly-D,L- lactide (R203 Boehringer Ingelheim), molecular weight 16,000 is used as the biodegradable polymer.

10

The potency of the test product is determined by HPLC by the manner outlined in USP. Release characteristics of the test product are established prior to commencement of the study, using the *in vitro* test procedure described in Example 10. The test product is shown to exhibit the following *in vitro* release:

15

Time (hr)	% release
1	10-40
4	20-60
8	40-80
16	>80

20

2 x 37.5 mg captopril containing amounts of the formulation are administered to volunteers (humans). Capoten (Trade Mark) (Squibb), is used as the reference in this study. Captopril microfluidised microcapsules/nanoparticles, as prepared in accordance with Example 8, as indicated above, are suitable for a once-daily preparation.

25

EXAMPLE 12***In-vitro* release from Hydromorphone loaded microcapsules**

5 Hydromorphone microspheres were prepared using a double emulsion technique as follows:

TABLE 8		
	Lot No.	
	Hm32	Hm30
R206 (poly-D,L-lactide; mw 109,000)	3.0 g	3.0 g
Hydromorphone HCl	0.3 g	0.3 g
Methylene Chloride	6.0 ml	8.0 ml
Gold gelatin (pharmaceutical grade)	1.0 ml	1.0 ml
Tris buffer (0.27% PVA; pH 9)	50.0 ml	50.0 ml
Acetone	----	3 ml
Actual Hydromorphone loading	4.80%	3.06%
Average size		

10 R206 polymer was dissolved in the solvent methylene chloride and hydromorphone was dissolved in the gelatin. The drug/gelatin mixture was emulsified into the polymer/solvent (S10 homogenizing shaft size/13,5000 for 2_ min for Hm32 and 2 min for Hm30). The resulting emulsion was itself emulsified into the aqueous Tris buffer (S25 homogenizing shaft size/13500 for 3_ min for Hm32 and 3 min for Hm30) to form microcapsules. The Hm32 microcapsules were stirred

1,000 rpm for 1_ hours to harden the microcapsules. The Hm30 microcapsules were stirred at 1,200 rpm for 15 minutes, the acetone was added and the mixture again stirred at 1,200 for an additional 1_ hours. The microcapsules were recovered by centrifuging at 13,500 rpm for 15
5 minutes and drying under a vacuum. The microcapsules were from 20-30 mm in diameter. Fig. 9 shows the dissolution of hydromorphone from these hydromorphone microspheres encased in gelatin capsules in simulated gastric fluid (0.1 M HCl).

EXAMPLE 13

10 *In-vitro* release from Nifedipine loaded microcapsules

Nifedipine loaded microspheres, with loadings up to 50% w/w drug loading using either R203 (poly-D,L-lactide; 16000 mw) or RG 504 (poly-D,L-lactide-co-glycolide; 50:50) were prepared using a procedure similar to that of Example 8 for diltiazem base loaded microspheres.
15 The microspheres were < 5 mm in diameter with entrapment efficiencies greater than 90% in all cases. As shown in Fig. 10, the release under sink conditions of nifedipine from 50% loaded R203 and 50% loaded RG 504 microspheres are compared to the release of nifedipine from 30% loaded R203 and 50% loaded RG 504 microspheres that were
20 mixed with lactose and tabletted prior to dissolution runs (Nifed retard, Rowa Pharmaceutical, as a control) over a period of 25 hours.

EXAMPLE 14

Effervescent Formulations

The following diltiazem effervescent formulations were prepared
25 from the microcapsule preparations of this invention similar to Example 8:

TABLE 9						
Lot No.						
wt% of final product	EFF6	EFF9	EFF10	EFF16	EFF19	EFF24
Diltiazem microspheres	5.0 (20% loading)	10.0 (20% loading)	10.0 (20% loading)	5.0 (20% loading)	12.0 (50% loading)	12.0 (20% loading)
Sodium bicarbonate	40.0	40.0	40.0	20.0	40	40
Potassium bicarbonate	---	---	---	22.5	---	---
Citric acid anhydrous	25.0	17.0	20.0	28.5	25.0	25.0
Sorbitol	10.0	---		18.0	---	---
Aspartame	10.0	10.0	10.0	5.0	10.0	10.0
Explotab	10.0	10.0	17.0	---	5.0	---
Kollidon 30	---	10.0	---	---	---	---
Starch	---	---	---	---	5.0	---
Methocel	---	---	---	---	---	5.0
Avicel pH 101	---	---	---	---	---	8.0
Flavour	---	3.0	3.0	3.0	3.0	
Tablet wt	1.0 g	1.0 g	1.0 g	1.0 g	1.0 g	1.0g

5 The microspheres of formulation EFF 6 were initially coated by spraying the microcapsules with a 1% solution of sodium docusate. The coated microspheres were dried in a vacuum oven overnight and dry blended with the other listed excipients and tabletted.

The ingredients of formulation EFF 9, EFF 16 and EFF 19 were dry-blended together and tabletted.

5 The microspheres of EFF 10 were blended with the acid and base phases and a wet granulation was prepared using a 1% solution of sodium docusate. The granulate was dried in the vacuum oven overnight and ground to a powder. The granulate was blended with the remaining dry excipients and tabletted.

10 A wet granulate was prepared from the microspheres, Methocel and the acid and base components using a 5% heated sodium docusate solution as the granulating agent in EFF 24. The granulate was dried under vacuum and ground to powder form. The granulate was blended with the remaining dry excipients and tabletted.

15 These effervescent formulations contain diltiazem base loaded microcapsules similar to those given in Example 8, whose general release properties in various pH environments are given in Figs. 5-7 and accompanying text and whose bioavailability results are outlined in Fig. 8 and accompanying text. As shown in Figs. 5-7 (e.g., release profiles at pH 7.4 and pH 1.2), the aqueous solubility of the diltiazem increases at pHs below its pK_a (around 8), with an appreciable increase in solubility and release observed at pHs < 7. Thus, effervescent formulations
20 containing diltiazem base desirably are adjusted to have a suspension pH of 7 or above to prevent the burst release of diltiazem in the suspension or in the subject prior to reaching the much more acidic environment of the stomach. By controlling the pH of the suspended effervescent
25 formulation, the release of diltiazem will be minimized until the diltiazem is delivered to absorption sites for diltiazem (e.g., stomach, small intestine). In this way, delivery of diltiazem can be optimized while still maintaining a desirable controlled, sustained release with a formulation that has the advantages inherent in a effervescent dosage
30 form.

The pH of effervescent formulations can be manipulated from about pH 5 to pH 8 by, for instance, increasing the relative amount of

sodium bicarbonate (to raise the pH) or increasing the citric acid component (to lower the pH). For instance, the diltiazem formulations of Table 9 can be adjusted to around pH 7.4 to minimize the burst effect of the microcapsules in the effervescent drink solution.

5 Similar effervescent formulations can also be formulated at appropriate pHs for nifedipine, captopril, hydromorphone etc. to advantageously optimize their bioavailability when administered orally to the subject. For instance, because nifedipine is very poorly water
10 soluble with its solubility increasing only at pHs < 2-3, incorporation of nifedipine loaded microcapsules into an effervescent matrix should not negatively affect its release properties. That is, negligible drug will be released in the effervescent drink (burst effect) prior to oral intake and thus the majority of the nifedipine will be delivered in a controlled
15 manner to the site(s) of its absorption. On the other hand, hydromorphone has a high aqueous solubility around effervescent solutions of around neutral pH and, therefore, release will have started to a certain extent prior to intake. Alternatively, the pH of the
20 hydromorphone effervescent formulation can be raised to about pH 8 to reduce the burst effect or the formulation's pH can be lowered below approximately pH 6 and the microcapsules can be coated or sprayed with an enteric coating to prevent drug release until after they pass through the stomach.

 Effervescent formulations containing more than one type of drug loaded microcapsules are also envisioned by this invention. That is,
25 microcapsules containing the same drug, for instance faster and slower releasing diltiazem microcapsules, can be combined in one effervescent formulation to improve the controlled sustained release profile for diltiazem. Alternatively, microcapsules containing different drugs, such as a calcium channel blocker (e.g., diltiazem, nifedipine) and a narcotic
30 analgesic (e.g., hydromorphone) can be formulated in one effervescent formulation to simultaneously provide optimized delivery of both drugs in the patient friendly effervescent dosage form. That is, using diltiazem/hydromorphone as an example, microcapsules with the desired release profile for diltiazem (e.g., *in vitro* release in simulated gastric

fluid) and formulated with hydromorphone loaded microcapsules in an effervescent formulation having a pH near or above pH 7 such as at pH 7.4. By selecting this relatively high pH for an effervescent drink solution, the delivery of diltiazem can be optimized without affecting the delivery profile of hydromorphone negatively.

Claims: -

1. An effervescent pharmaceutical formulation for the sustained and controlled oral administration of a pharmaceutically effective amount of a drug selected from a calcium channel blocker, an
5 ACE inhibitor, a narcotic analgesic or analogues combinations thereof, said formulation comprising microcapsules in which the drug is entrapped in a biodegradable polymer.
2. An effervescent pharmaceutical formulation according to Claim 1, wherein, the pH of the formulation allows for optimized
10 delivery of the or each drug.
3. An effervescent pharmaceutical formulation according to Claim 1 or 2, wherein the formulation is used to deliver the drug to a patient on a once-daily basis so as to achieve a therapeutic effect over a substantially 24 hour period.
- 15 4. An effervescent pharmaceutical formulation according to any preceding claim, wherein the microcapsules have a D 50% between about 100 nm and 900 nm.
5. An effervescent pharmaceutical formulation according to any preceding claim, wherein the drug loading of the microcapsules
20 ranges from about 10% to 70% by weight.
6. An effervescent pharmaceutical formulation for the sustained and controlled oral administration of a pharmaceutically effective amount of a drug selected from a calcium channel blocker, an ACE inhibitor, a narcotic analgesic or a combination thereof, the
25 formulation comprising drug-loaded biodegradable microcapsules having a D 50% between about 100 nm and 900 nm and a drug loading which ranges from about 10% to 70% by weight and wherein the pH of the formulation is adjusted to optimize delivery of the or each drug.

7. An effervescent pharmaceutical formulation according to Claim 6, which can be used to deliver the drug to a patient on a once-daily basis so as to achieve a therapeutic effect over a substantially 24 hour period.

5 8. An effervescent pharmaceutical formulation according to any preceding claim, wherein the microcapsules have a D 50% between about 200 nm and 400 nm.

9. An effervescent pharmaceutical formulation according to any preceding claim, wherein the drug loading of the microcapsules
10 ranges from about 20% to 50% by weight.

10. An effervescent pharmaceutical formulation according to to any preceding claim, wherein the drug is selected from diltiazem, verapamil, nifedipine, nimodipine, nicardipine, hydromorphone, codeine sulfate, oxycodone, dihydrocodeine tartrate, oxycodone, morphine,
15 fentanyl, sufentanil, oxymorphone, buprenorphine, captopril, enalapril, lisinopril and mixtures thereof.

11. An effervescent pharmaceutical formulation according to Claim 10, wherein the drug is a mixture of nifedipine and hydromorphone.

20 12. A pharmaceutical formulation according to any preceding claim, wherein the polymer matrix comprises polylactide; polyglycolide; poly(lactic acid-co-glycolic acid); poly(ϵ -caprolactone); poly(hydroxybutyric acid); polyortho-esters; polyacetals; polydihydropyrans; polycyanoacrylates; polypeptides; cross-linked
25 polypeptides; and stereoisomers, racemic mixtures, co-polymers and polymer mixtures thereof.

13. A pharmaceutical formulation according to Claim 12, wherein the polymer matrix comprises poly-D,L-lactide.

14. A pharmaceutical formulation according to any preceding claim, wherein the release profile measured in accordance with the Paddle Method of U.S. Pharmacopoeia XX at 37°C and 75 rpm for the or each drug is substantially as follows:

- 5 a) 10-30% release within 2 hours after administration;
- b) 30-60% release within 4 hours after administration;
- c) 60-80% release within 8 hours after administration; and
- d) $\geq 80\%$ release within 24 hours after administration.

10 15. A pharmaceutical formulation according to any one of Claims 1-13, wherein the release profile measured in accordance with the Paddle Method of U.S. Pharmacopoeia XX at 37°C and 75 rpm for the or each drug is substantially as follows:

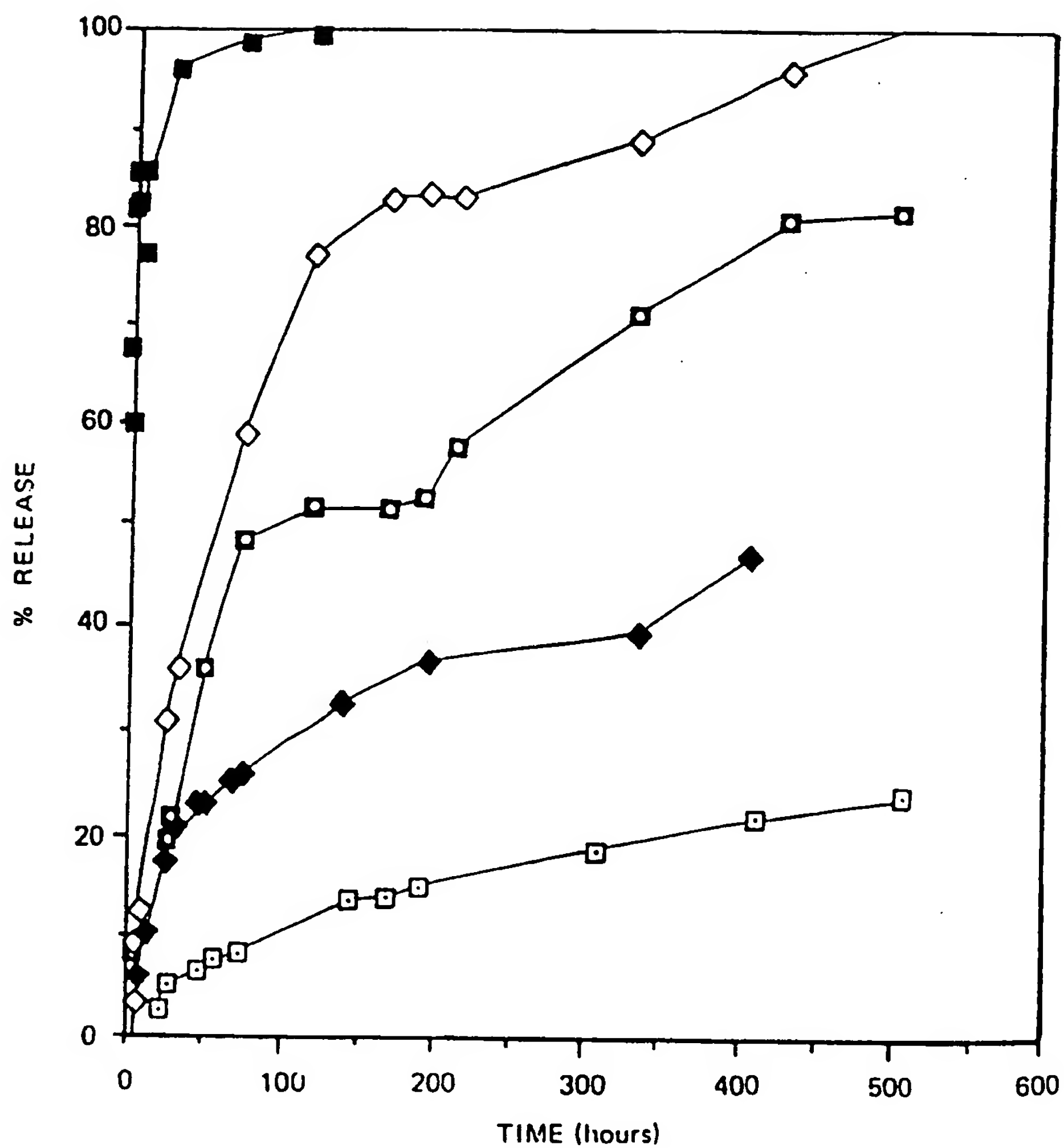
- a) 10-40% release within 1 hour after administration;
- b) 20-60% release within 4 hours after administration;
- 15 c) 40-80% release within 8 hours after administration; and
- d) $\geq 80\%$ release within 16 hours after administration.

16. A method for the manufacture of microcapsules according to any one of Claims 1-15, which comprises the steps of:

- 20 a) dissolving or dispersing a drug and a biodegradable polymer in a solvent to form a mixture;
- b) microfluidising said mixture into an external phase to form an emulsion in which the emulsion droplets have a mean diameter less than 1 mm; and

- c) stirring said emulsion to form microcapsules having a size (D 50%) between about 100 nm and 900 nm.

1/10



—■— DILTIAZEM
—□— D1
—◆— D2
—□— D3
—◇— D4

FIG. 1

2/10

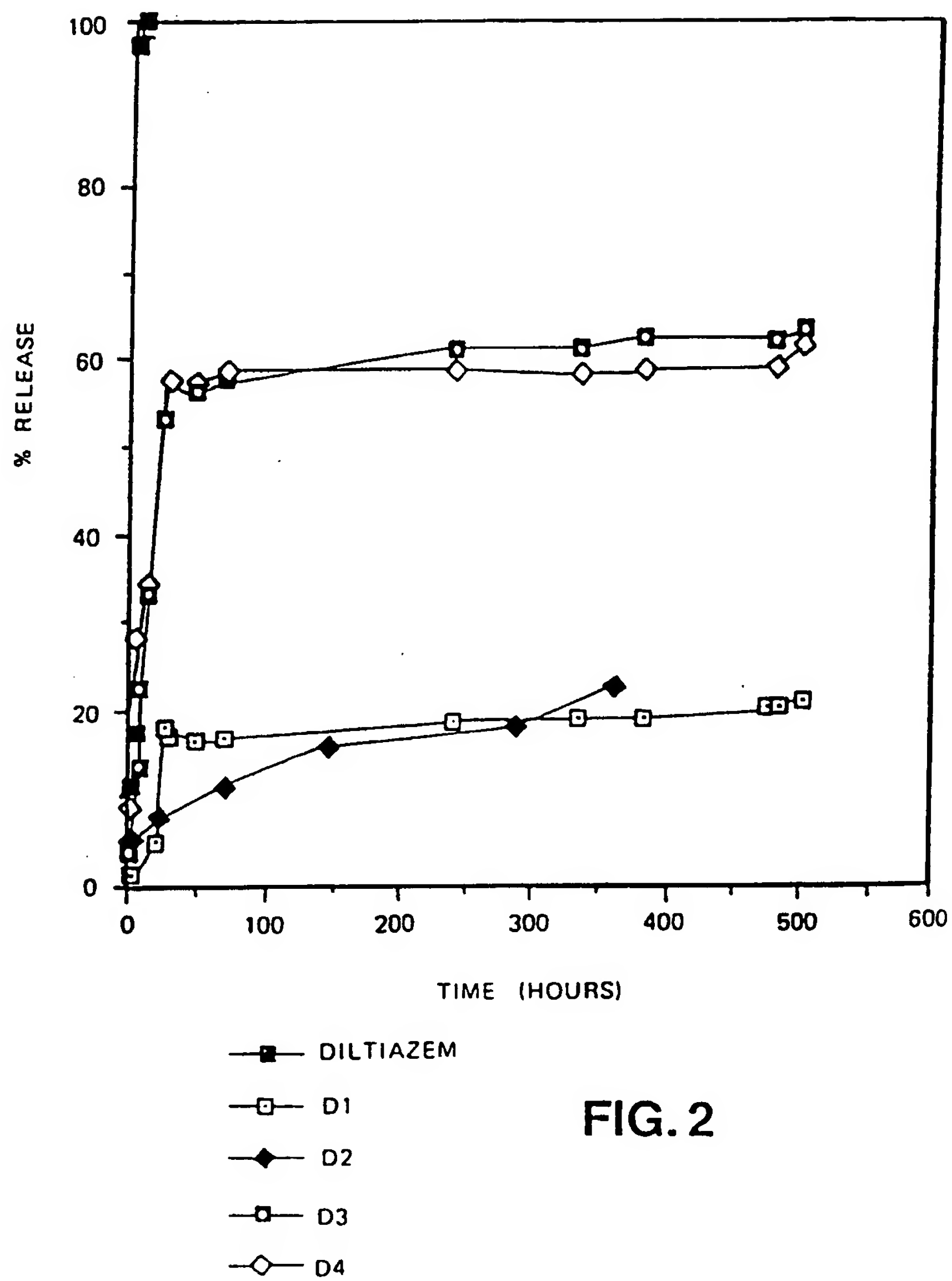


FIG. 2

3/10

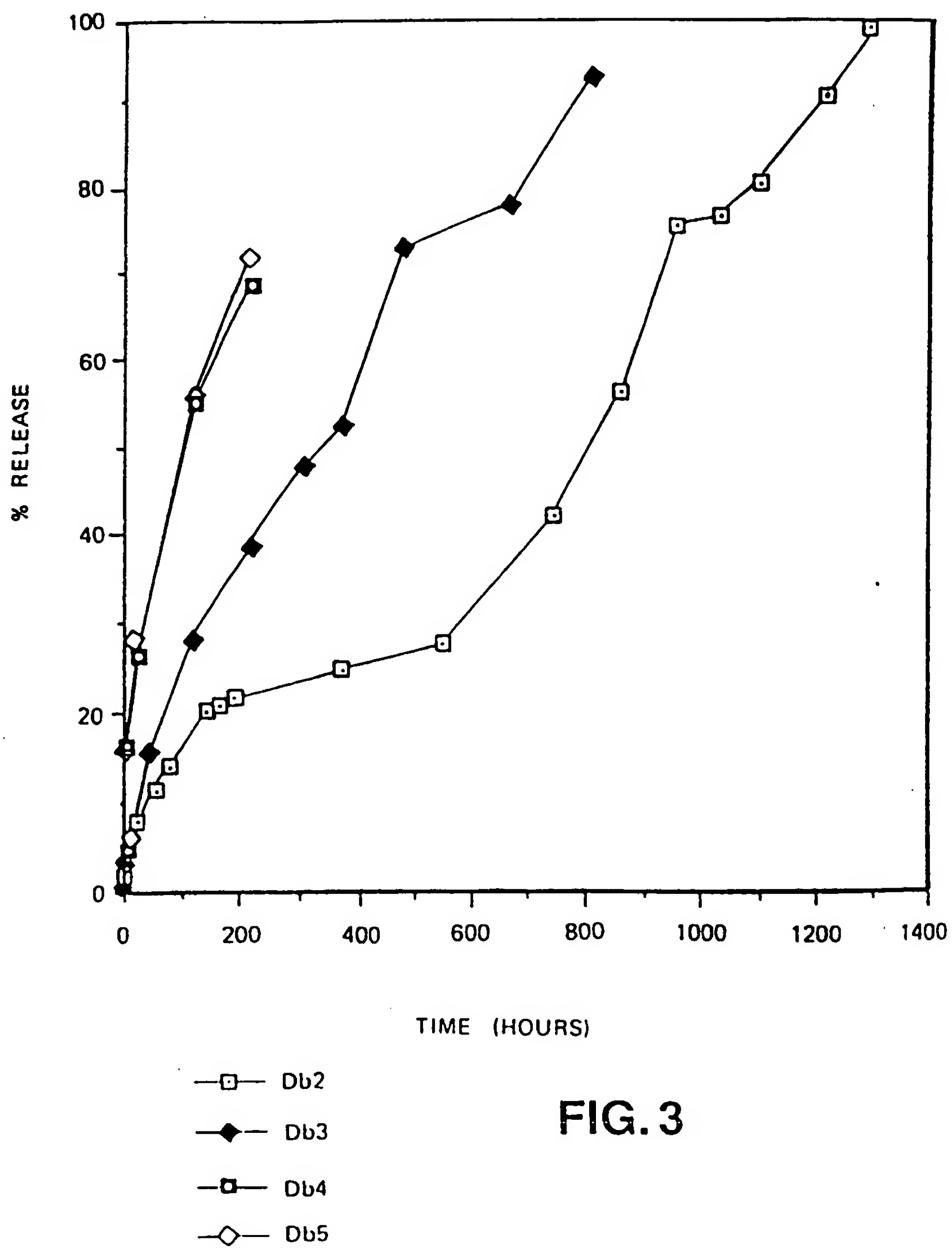


FIG. 3

4/10

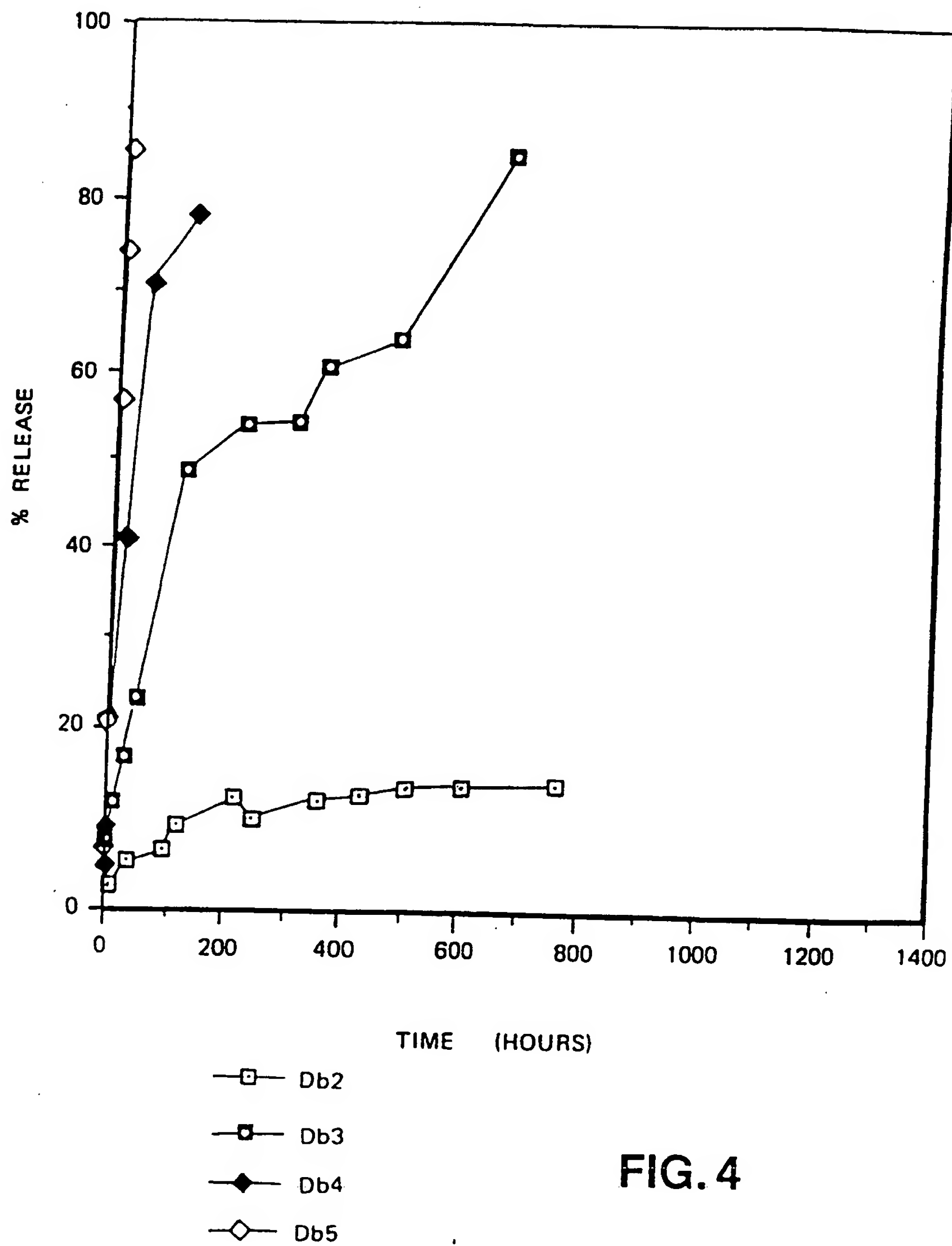
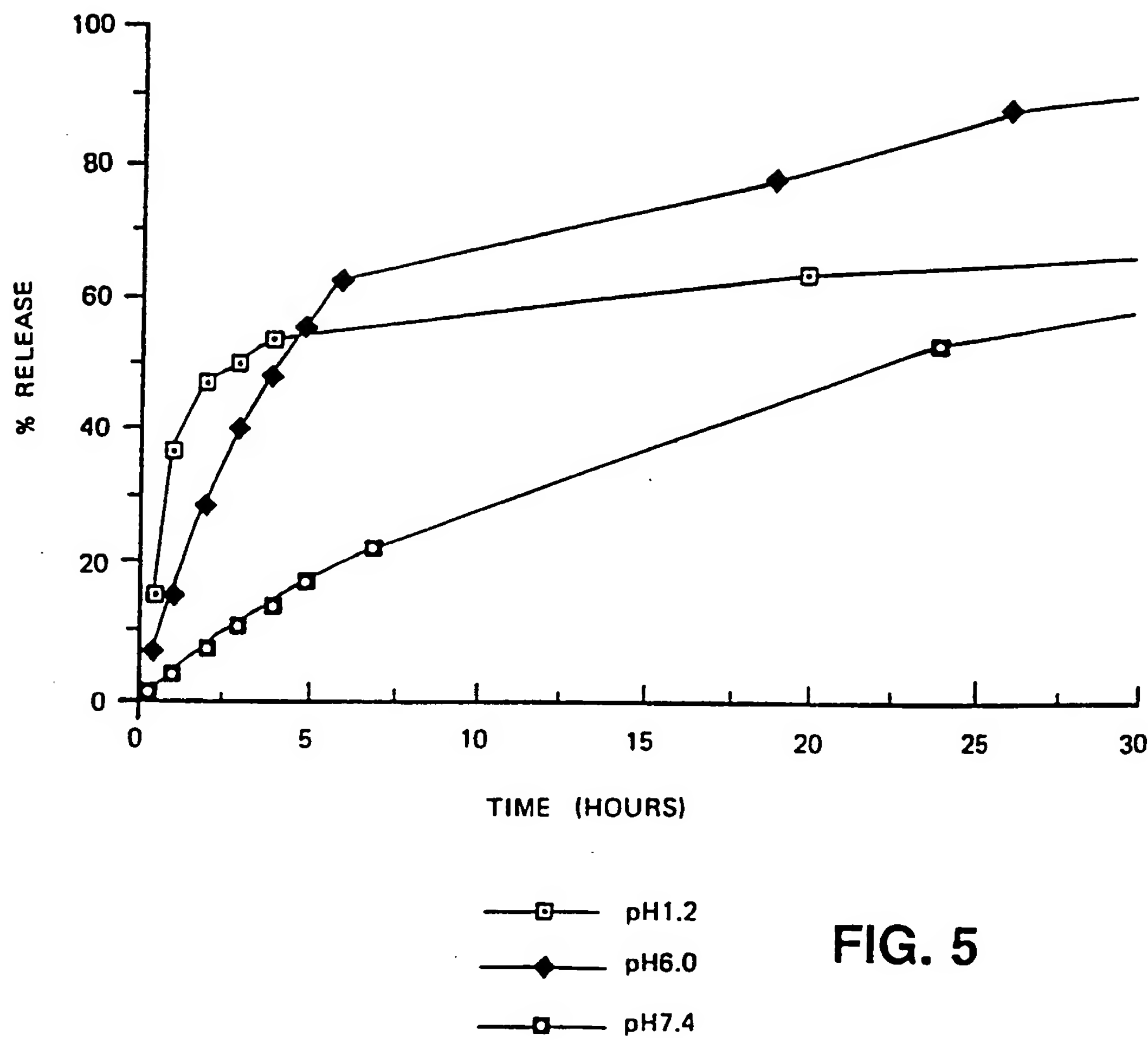
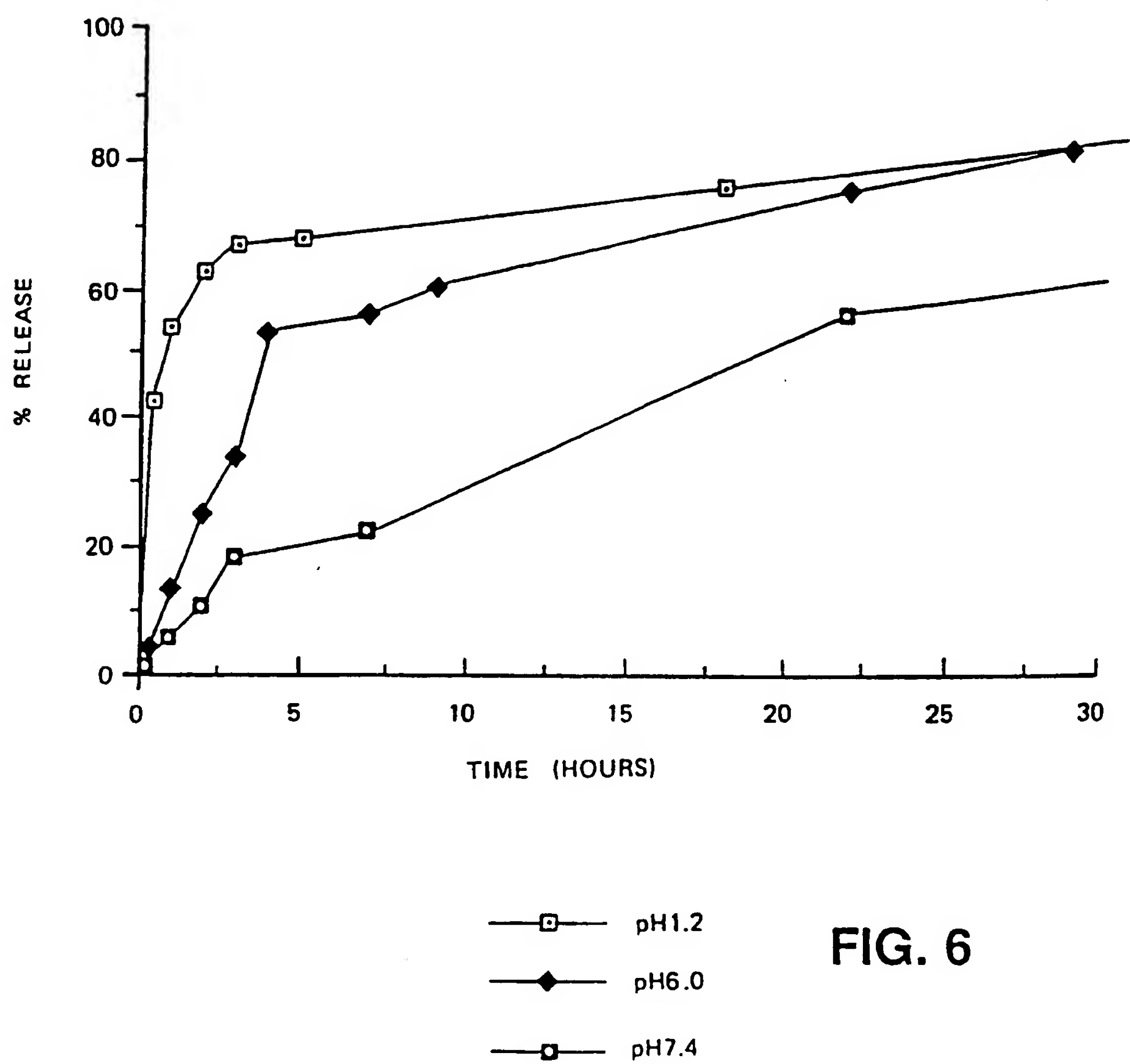


FIG. 4

5/10



6/10



7/10

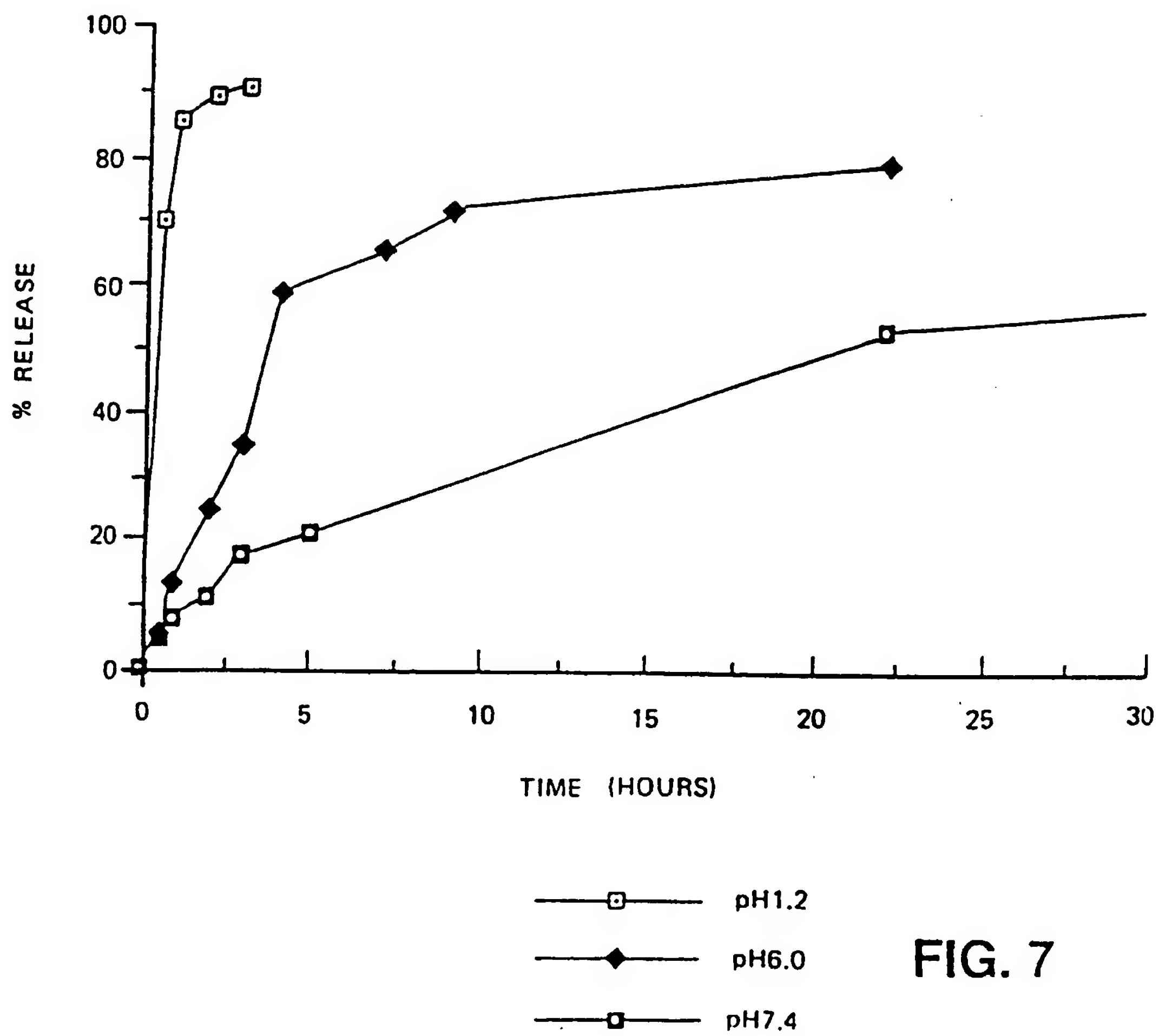
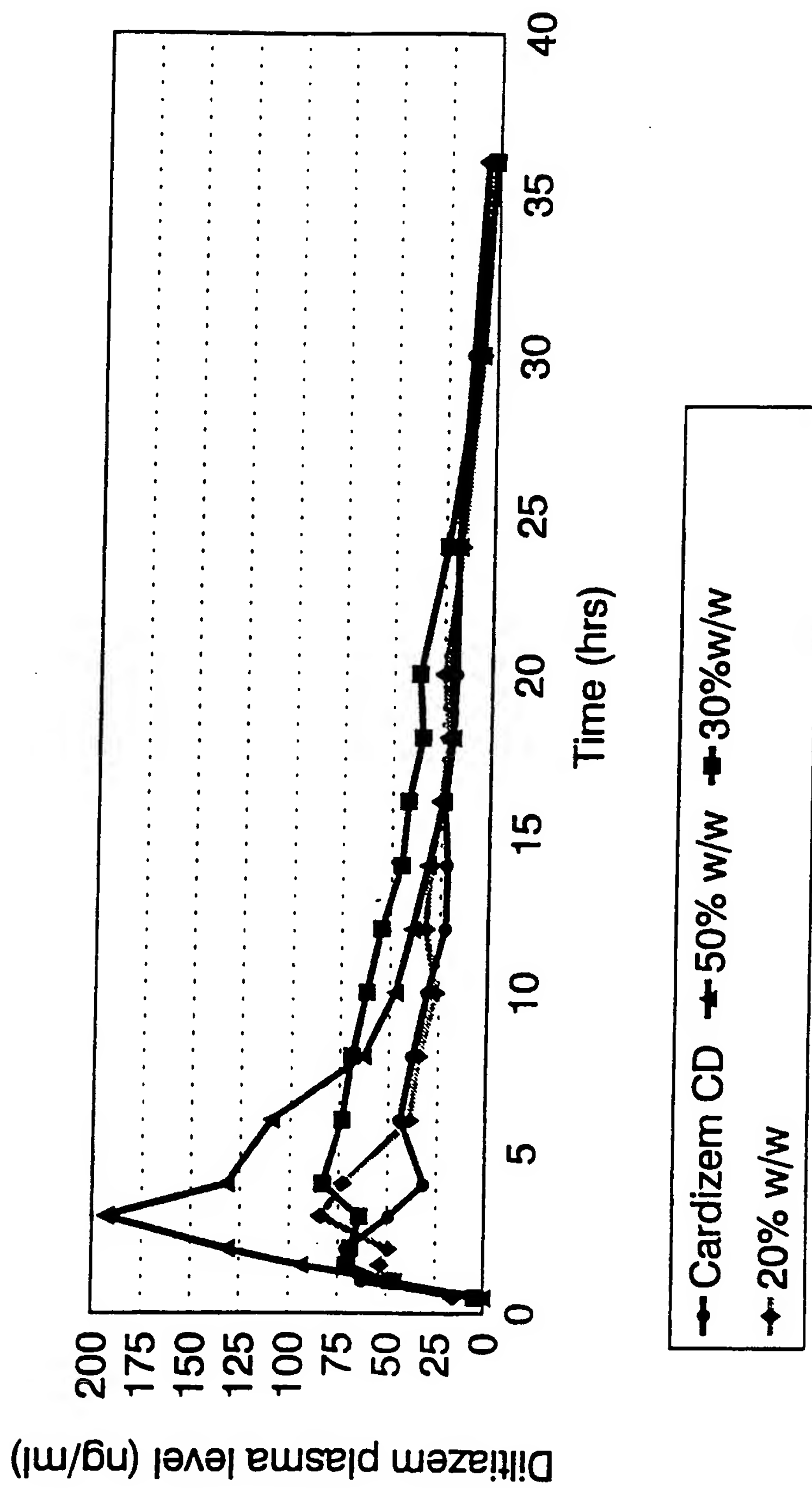
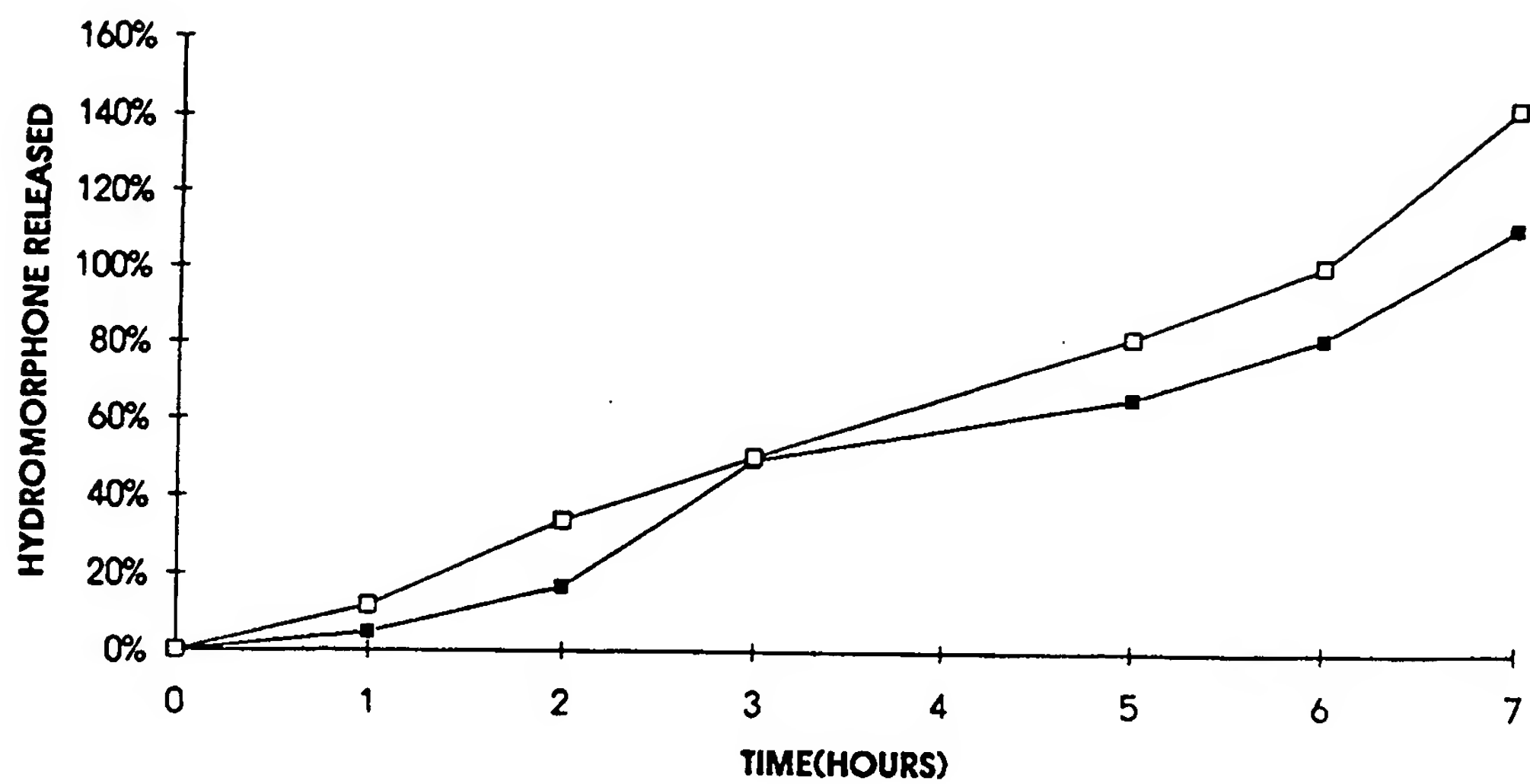


Figure 8



9/10

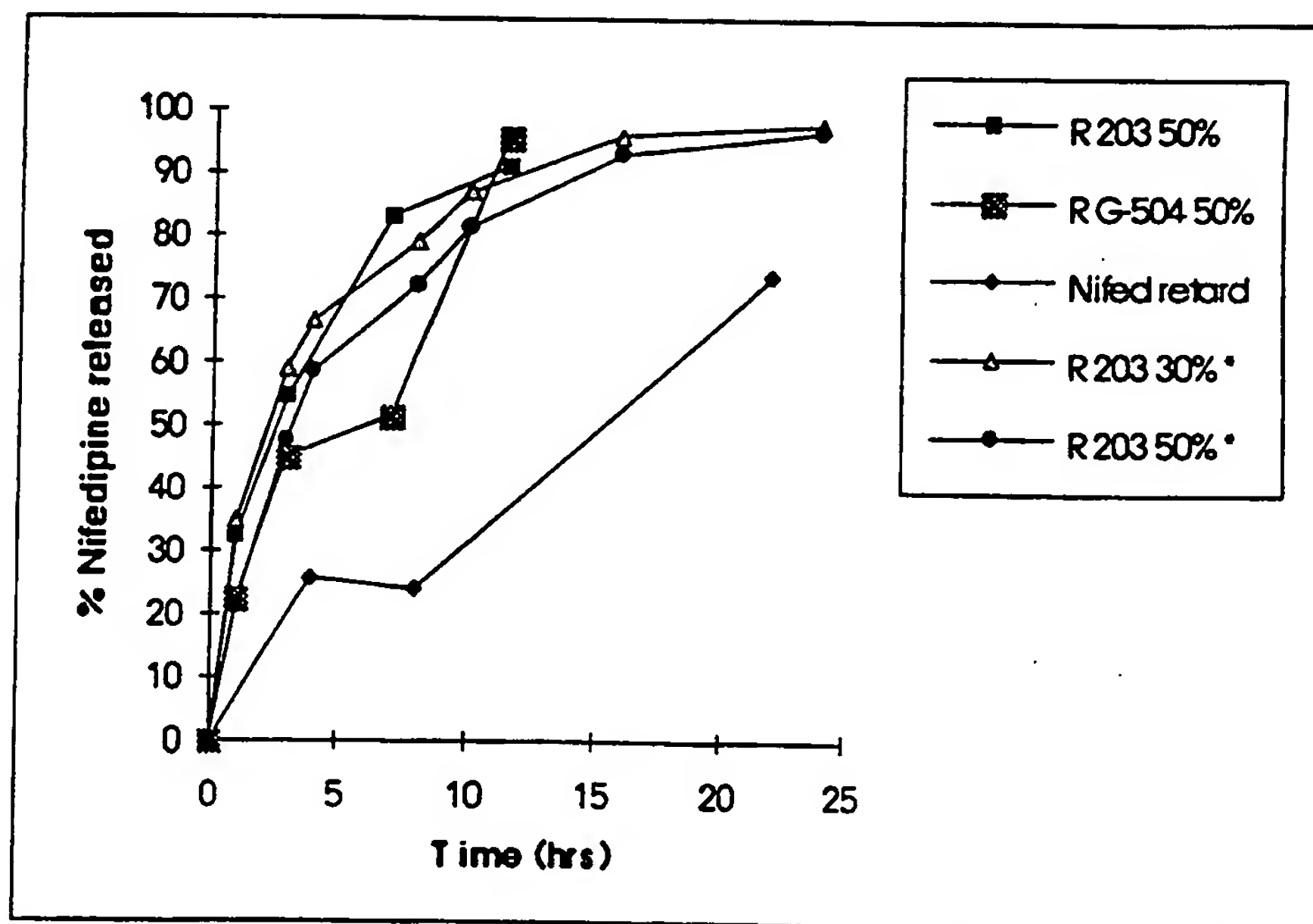
FIGURE 9



—■— Hm30
—□— Hm32

10/10

FIGURE 10



INTERNATIONAL SEARCH REPORT

International Application No.
PCT/IE 95/00025

A. CLASSIFICATION OF SUBJECT MATTER

A 61 K 9/51, A 61 K 9/52, A 61 K 9/46, A 61 K 9/56,
A 61 K 9/58, A 61 K 9/64

According to International Patent Classification (IPC) or to both national classification and IPC 6

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

A 61 K

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	EP, A, 0 257 310 (BIO-DAR LTD.) 02 March 1988 (02.03.88), claims 1,2,4; column 6, lines 50-56; column 3, line 50 - column 4, line 4.	1-3
X	EP, A, 0 145 240 (TAKEDA CHEMICAL INDUSTRIES, LTD.) 19 June 1985 (19.06.85), abstract; claims 1,4-6,10; page 2, lines 13-23; page 6, lines 1-12; page 7, lines 1-3; page 9, lines 10-22; page 10, line 36 - page 11, line 20;	1-3, 5, 9, 10, 12, 13

☒ Further documents are listed in the continuation of box C.☐ Patent family members are listed in annex.

* Special categories of cited documents :

- "A" document defining the general state of the art which is not considered to be of particular relevance
"E" earlier document but published on or after the international filing date
"L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)
"O" document referring to an oral disclosure, use, exhibition or other means
"P" document published prior to the international filing date but later than the priority date claimed

- "T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention
"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone
"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.
"&" document member of the same patent family

Date of the actual completion of the international search
23 May 1995

Date of mailing of the international search report

03. 07. 95

Name and mailing address of the ISA

European Patent Office, P.B. 5818 Patentlaan 2
NL - 2280 HV Rijswijk
Tel. (+31-70) 340-2040, Tx. 31 651 epo nl,
Fax (+31-70) 340-3016

Authorized officer

MAZZUCCO e.h.

C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT.		
Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
	page 17, lines 1-9. --	
Y	EP, A, 0 330 180 (BIOMATERIALS UNIVERSE, INC.) 30 August 1989 (30.08.89), abstract; claims 1-6; page 3, line 38 - page 4, line 32; page 5, lines 36-51. --	1-10, 12,13, 16
Y	US, A, 5 178 878 (WEHLING F. et al.) 12 January 1993 (12.01.93), claims 1,6; column 2, lines 59-65; column 3, lines 45-48; column 4, lines 56-62; column 5, lines 51-62; column 11, lines 38-50 (cited in the application). --	1-10, 12,13, 16
Y	US, A, 5 133 908 (STAINMESSE S. et al.) 28 July 1992 (28.07.92), abstract; claims 1,2,6,7; column 6, example 4; column 2, line 27 - column 3, line 18; column 3, lines 27-33; column 11, lines 42,43. --	1-10, 12,13
Y	US, A, 4 824 675 (WONG P.S.L. et al.) 25 April 1989 (25.04.89), claims 1,4,7; fig. 2; column 2, line 31 - column 3, line 12; column 12, line 38 - column 13, line 3; column 13, lines 30-49; column 14, lines 38-47; column 14, lines 64,65; column 15, line 67 - column 16, line 9; column 16, line 35 - column 17, line 46. --	1-10, 12,13
A	DE, A, 2 146 174 (MERCK & CO., INC.) 30 March 1972 (30.03.72), claims 1,10,11; page 2, fifth paragraph - page 4, line 3, examples 5,6; example 28. ----	1,3,12

ANHANG

ANNEX

ANNEXE

zum internationalen Recherchen-
bericht über die internationale
Patentanmeldung Nr.

to the International Search
Report to the International Patent
Application No.

rapport de recherche inter-
national relatif à la demande de brevet
international n°

PCT/IE 95/00025 SAE 107574

In diesem Anhang sind die Mitglieder
der Patentfamilien der im obenge-
nannten internationalen Recherchenbericht
angeführten Patentdokumente angegeben.
Diese Angaben dienen nur zur Unter-
richtung und erfolgen ohne Gewähr.

This Annex lists the patent family
members relating to the patent documents
cited in the above-mentioned inter-
national search report. The Office is
in no way liable for these particulars
which are given merely for the purpose
of information.

La présente annexe indique les
membres de la famille de brevets
relatifs aux documents de brevets cités
dans le rapport de recherche inter-
national visée ci-dessus. Les renseigne-
ments fournis sont donnés à titre indica-
tif et n'engagent pas la responsabilité
de l'Office.

Im Recherchenbericht angeführtes Patentdokument Patent document cited in search report Document de brevet cité dans le rapport de recherche	Datum der Veröffentlichung Publication date Date de publication	Mitglied(er) der Patentfamilie Patent family member(s) Membre(s) de la famille de brevets	Datum der Veröffentlichung Publication date Date de publication
EP A1 257310	02-03-88	CA A1 1312283	05-01-93
		DE C0 3775858	20-02-92
		EP B1 257310	08-01-92
		JP A2 2072113	12-03-90
		US A 4710384	01-12-87
EP A2 145240	19-06-85	AT E 42197	15-05-89
		CA A1 1233414	01-03-88
		DE C0 3477732	24-05-89
		EP A3 145240	03-07-85
		EP B1 145240	19-04-89
		ES A1 537325	01-04-86
		ES A5 537325	03-05-86
		ES A1 8605983	01-10-86
		GR A 80818	04-03-85
		HK A 37792	17-01-92
		HU A2 37037	28-11-85
		HU B 193910	28-12-87
		IE B 57721	24-03-93
		JP A2 60100516	04-06-85
		JP B4 1057087	04-12-89
		PT A 79450	01-12-84
		PT B 79450	11-12-86
		SG A 1034791	17-01-92
		US A 4652441	24-03-87
		US A 4711782	08-12-87
		US A 4917893	17-04-90
		US A 5061492	29-10-91
EP A1 330180	30-08-89	DE C0 68904326	25-02-93
		DE T2 68904326	27-05-93
		EP B1 330180	13-01-93
		JP A2 1216918	30-08-89
		US A 5100669	31-03-92
US A 5178878	12-01-93	AU A1 66012790	28-04-91
		AU B2 646232	17-02-94
		EP A1 494972	22-07-92
		EP A4 494972	12-08-92
		JP T2 5500956	25-02-93
		WO A1 9104757	18-04-91
		US A 5223264	29-06-93
		CA AA 2061917	27-08-93
US A 5133908	28-07-92	AT E 84710	15-02-93
		DE C0 68904483	04-03-93
		DE T2 68904483	19-05-93
		EP A1 349428	03-01-90
		EP B1 349428	20-01-93
		ES T3 2054052	01-08-94
		FR A2 2634397	26-01-90
		FR B2 2634397	19-04-91
		JP A2 2149334	07-06-90
		JP B4 6002224	12-01-94
		AT E 74024	15-04-92
		CA A1 1292168	19-11-91
		DE C0 3777796	30-04-92
		EP A1 275796	27-07-88
		EP B1 275796	25-03-92
		ES T3 2031151	01-12-92
		FR A1 2608988	01-07-88
		FR B1 2608988	11-01-91
		JP A2 63240936	06-10-88
		US A 5118528	02-06-92

US A	4824675	25-04-89	AU A1	16517/88	19-01-89
			AU B2	613040	25-07-91
			CA A1	1319071	15-06-93
			DE C0	3871273	25-06-92
			EP A2	300623	25-01-89
			EP A3	300623	22-03-89
			EP B1	300623	20-05-92
			ES T3	2031238	01-12-92
			JP A2	1031710	02-02-89
			US A	4915949	10-04-90
DE A	2146174	30-03-72	AU A1	33178/71	15-03-73
			FR A5	2106566	05-05-72
			FR B1	2106566	18-04-75
			NL A	7112083	20-03-72